

PROSEC APPLICATION EXAMPLE

SIMULATION OF A CROSS-FLOW PLATE-FIN HEAT EXCHANGER (PFHE) WITH CO- PROSEC CAPE-OPEN UNIT OPERATION

EXAMPLE PURPOSE

This example shows a cross-flow plate-fin heat exchanger used in a gas-gas application. This heat exchanger is modeled using CO-ProSec, Fives ProSim's CAPE-OPEN compliant unit operation dedicated to the simulation of plate-fin heat exchangers. Regarding the thermodynamic and physico-chemical data needed, they are automatically calculated using the thermodynamic calculation server of the process simulation software.

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CORRESPONDING PROSEC FILES

COPROSEC_EX_EN-Cross-flow-heat-exchanger.pmp3

Reader is reminded that this use case is only an example and should not be used for other purposes. Although this example is based on actual case it may not be considered as typical nor are the data used always the most accurate available. Fives ProSim shall have no responsibility or liability for damages arising out of or related to the use of the results of calculations based on this example.

Energy

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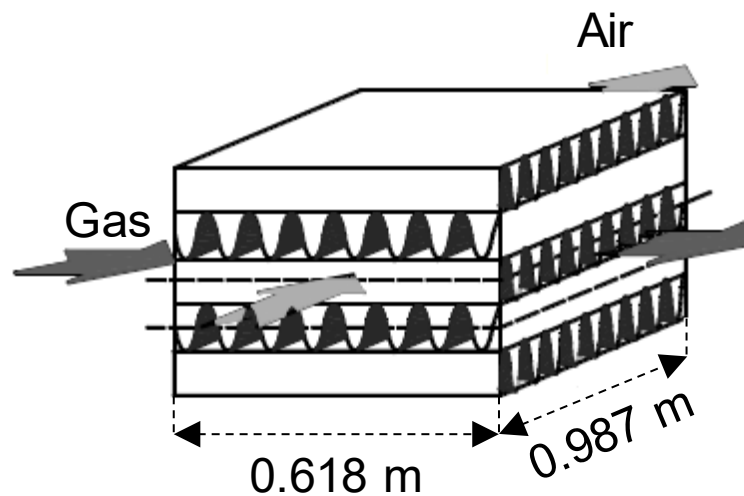
1. PROCESS MODELING

1.1. Process description

This example deals with a gas-gas cross-flow plate-fin heat exchanger (PFHE). Compact heat exchangers are characterized by a large heat transfer surface area per unit volume. Amongst different varieties of compact heat exchangers, cross-flow plate-fin heat exchangers are widely used in aerospace, automobile, cryogenic and chemical process plants for their low weight and volume, high efficiency. It will be simulated with CO-ProSec CAPE-OPEN unit operation. In CO-ProSec, cross-flow heat exchangers are modeled as pure counter-flow heat exchangers and an efficiency coefficient [ROE10] is computed and applied to take into account the cross-flow behavior. The assumptions of the model are:

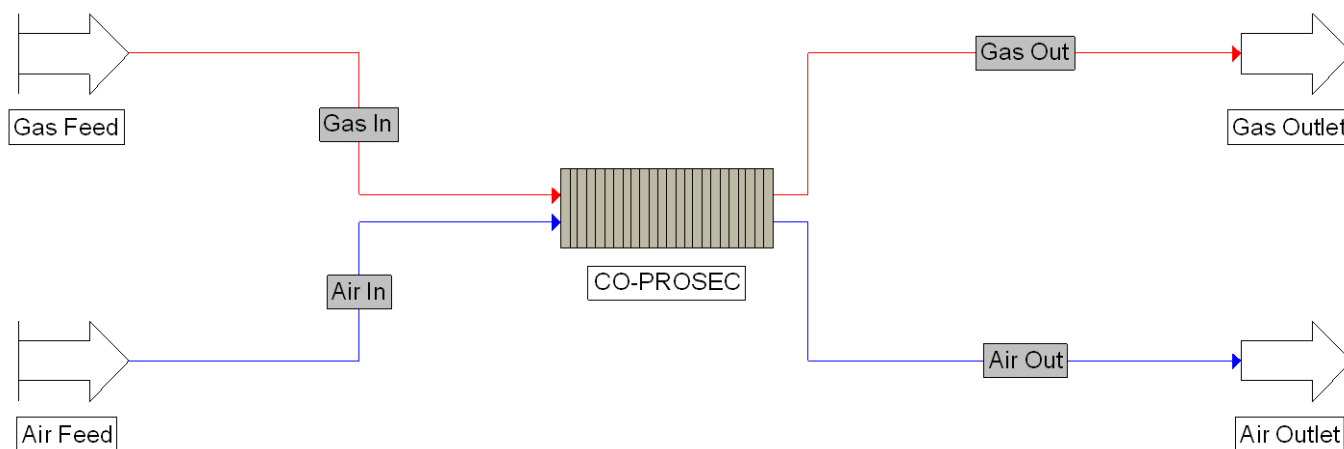
- ✓ Common wall temperature,
- ✓ Longitudinal conduction not taken into account,
- ✓ Two fluids,
- ✓ Continuous thermodynamic option not available.

The example is extracted from [MIS09]. The sketch of the heat exchanger is shown below. The two fluids are modeled as air. The “Gas” is the main stream and the “Air” is the cross-flow stream.



The thermodynamic and physico-chemical data needed for the simulation are automatically calculated by the unit operation. In this example, as the ProSec CAPE-OPEN unit operation is used in ProSimPlus simulation environment, it uses Simulis Thermodynamics, the calculation server for thermophysical properties and phase equilibria calculations available in ProSimPlus.

1.2. Process flowsheet



1.3. Compounds

The compounds taken into account in the simulation, their chemical formula and CAS numbers are shown in the following table. Their pure component properties are extracted from the standard database provided with ProSimPlus [ROW23].

Compound	Chemical formula	CAS number ¹
Oxygen	O ₂	7782-44-7
Nitrogen	N ₂	7727-37-9

1.4. Thermodynamic model

The PSRK profile, which is based on a predictive combined approach model [HOL91], [GME91], [CHE02] is selected.

1.5. Operating parameters

1.5.1. Process feed

	Gas	Air
Temperature (°C)	240	4
Pressure (bar)	1	1
Total flow rate (kg/s)	0.8962	0.8296
Molar fraction		
Oxygen	0.21	
Nitrogen	0.79	

¹ CAS Registry Numbers® are the intellectual property of the American Chemical Society and are used by Fives ProSim SAS with the express permission of ACS. CAS Registry Numbers® have not been verified by ACS and may be inaccurate.

1.5.2. Plate-fin heat exchanger

✓ General parameters

Parameters	Value
Type of exchanger	CO-ProSec
Number of body	1
Orientation	Horizontal
Fin data base	2015 -> Now
Material	
Type	Other
a1	160
a2 = a3 = a4 = a5 = a6 =a7	000
Used width (m)	0.987
Thickness of the side bars (mm)	0.001
Thickness of the end bars (mm)	0.001
Thickness of the separation plates (mm)	0.500
Thickness of the closing plates (mm)	0.500

✓ Streams parameters

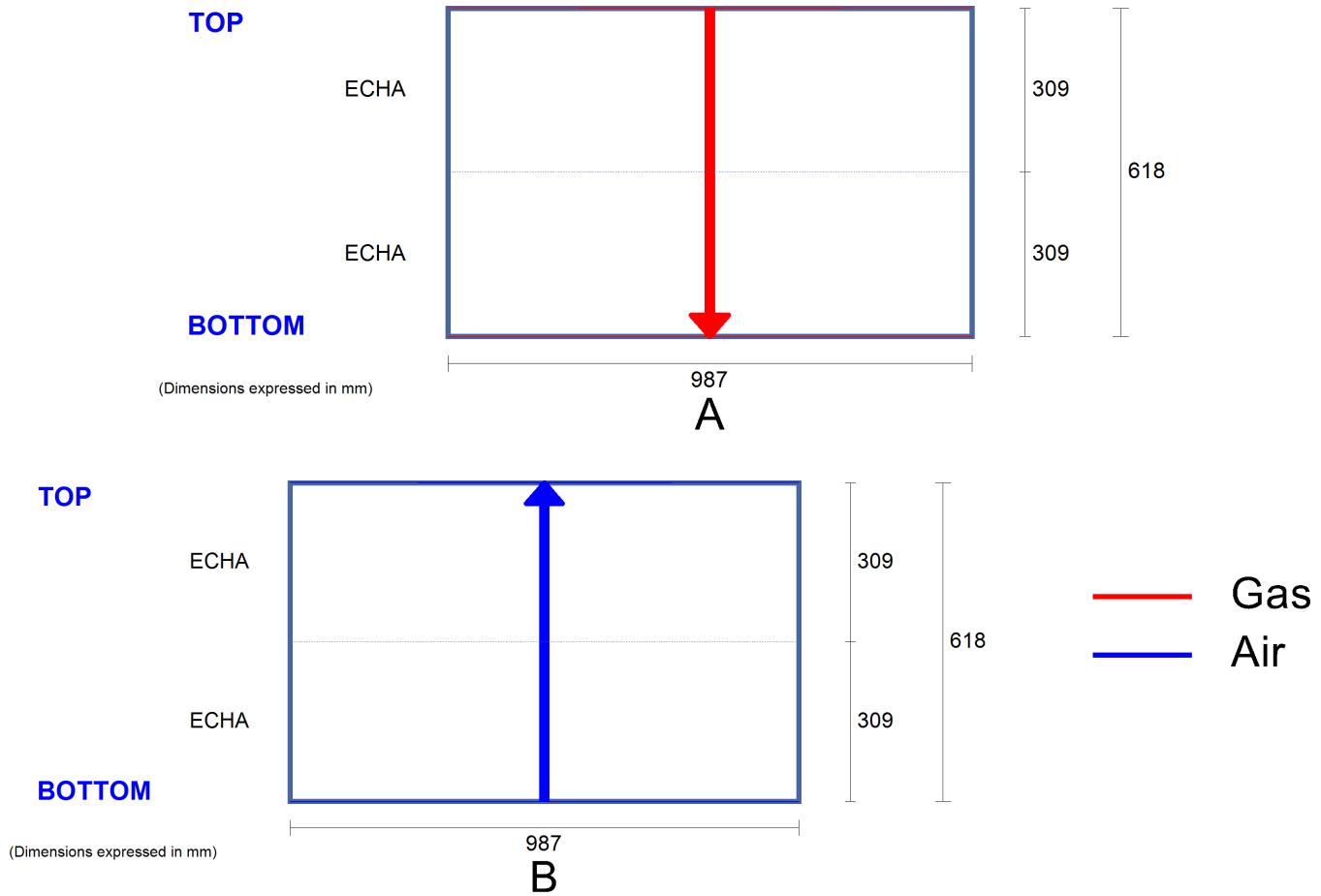
Parameter	Stream	
	Gas	Air
Flow direction	From top to bottom	From bottom to top
Cross flow	No	Yes
Heat exchange correlation	HTFS85	
Other parameters	Default values	

✓ Fin characteristics

Name	Fin #1
Origin	User
Calculation mode	From geometry
Reference	1001
Type	Serrated
Height (mm)	9.799
Thickness (mm)	0.101
Fins number per meter	654.5
Serration length (mm)	7.551
Other parameters	Default values

✓ Reference passages

Fin #1 is used for each stream. The following figures show the two reference passages of the heat exchanger. The dimensions are expressed in millimeter.



TOP

ECHA

ECHA

BOTTOM

(Dimensions expressed in mm)

987

618

309

309

B

Gas

Air

✓ Stacking

Parameters	Value
Sequence 1	
Number of repetitions of the sequence	9
Sequence	B A
Sequence 2	
Number of repetitions of the sequence	1
Sequence	B

- [TOP](#)

(6)	309
(12)	618

(Dimensions expressed in mm)

987

2. RESULTS

2.1. Mass and energy balances

Streams		Air In	Air Out	Gas In	Gas Out
Total flow (mass)	kg/s	0.8296	0.8296	0.8962	0.8962
Mole fractions					
OXYGEN		0.21	0.21	0.21	0.21
NITROGEN		0.79	0.79	0.79	0.79
Physical state		Vapor	Vapor	Vapor	Vapor
Temperature	°C	4	201.81	240	57.829
Pressure	kPa	100	95.282	100	97.998
Enthalpic flow	kW	-17.831	149.49	196.94	29.628
Molar vapor fraction		1	1	1	1

2.2. Global results

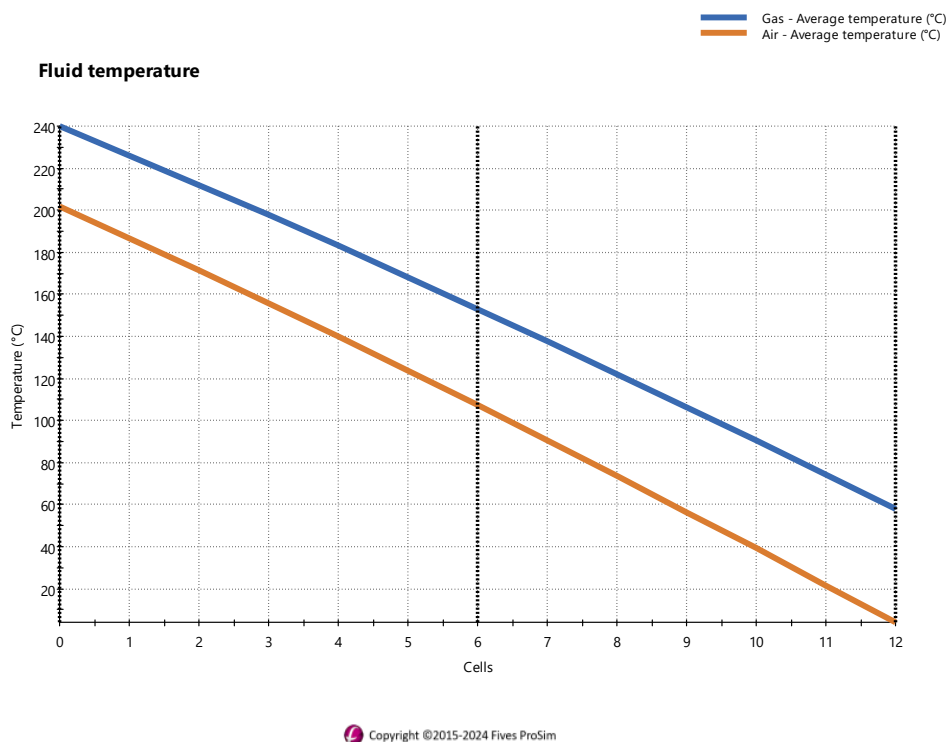
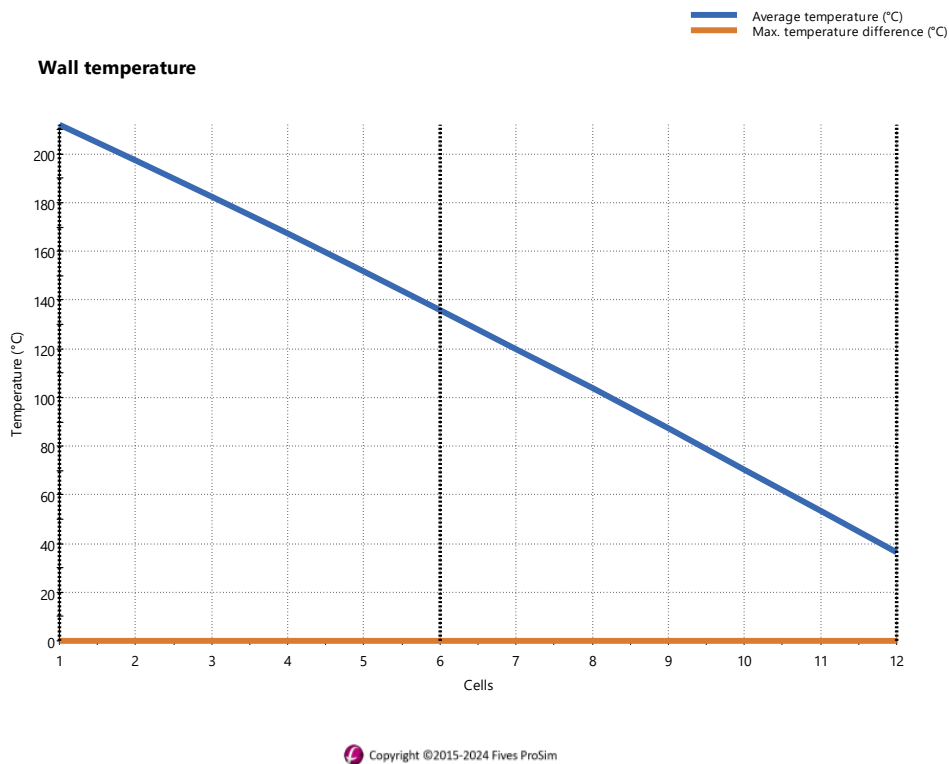
The heat duty computed by CO-ProSec is 167 kW. [MIS09] indicates a value of 160 kW. The deviation is explained by the differences in the assumptions:

- ✓ Constant physico-chemical properties for [MIS09] vs temperature dependent for ProSec,
- ✓ The correlations used to compute the Colburn and Fanning factors are not the same.

The pressure drops computed by ProSec (2 003 Pa for the gas stream and 4 718 Pa for the air stream) are close to the ones calculated by [MIS09].

2.3. Plate-fin heat exchanger profiles

Several profiles (wall temperature, fluid temperature, pressure, heat transfer coefficient, vaporization ratio...) in the heat exchanger are available after the simulation from ProSec edition window ("Results" tab). The following figures show the average wall temperature profile and the fluid mean temperature profiles along the length of the heat exchanger.



3. REFERENCES

- [CHE02] CHEN J., FISCHER K., GMEHLING J., "Modification of PSRK Mixing Rules and Results for Vapor – Liquid Equilibria, Enthalpy of Mixing and Activity Coefficients at Infinite Dilution", Fluid Phase Equilib., 200, 411-429 (2002)
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- [HOL91] HOLDERBAUM T., GMEHLING J., "PSRK: A Group Contribution Equation of State based on UNIFAC", Fluid Phase Equilib., 70, 251-265 (1991)
- [MIS09] MISHRA M., DAS P.K., "Thermoeconomic Design-Optimisation of Crossflow Plate-Fin Heat Exchanger Using Genetic Algorithm", Int. J. Exergy, 6, 837-852 (2009)
- [ROE10] ROETZEL W., SPANG B., "VDI Heat Atlas, Chapter C1: Thermal Design of Heat Exchangers", Springer-Verlag, 2nd Edition (2010)
- [ROW23] ROWLEY R.L., WILDING W.V., OSCARSON J.L., GILES N.F., "DIPPR® Data Compilation of Pure Chemical Properties", Design Institute for Physical Properties, AIChE (2023)