## Getting started with ProSec® in ProSimPlus® environment

#### Use Case 1: Main features overview

Software & Services In Process Simulation



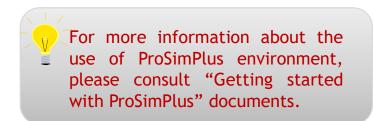
We guide You to efficiency

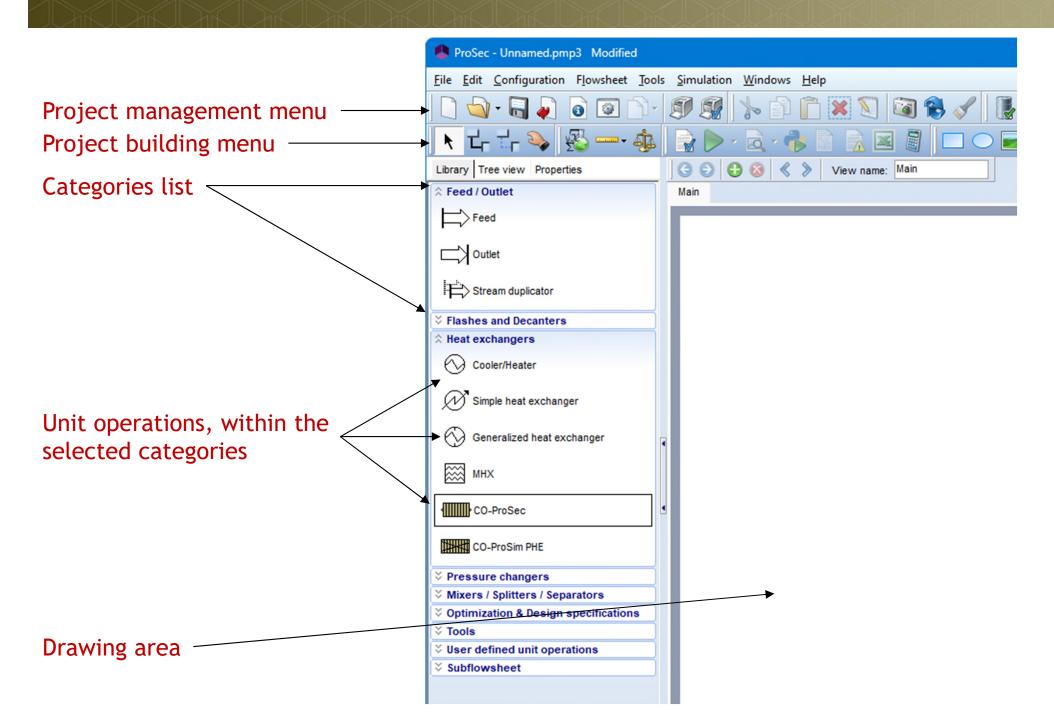
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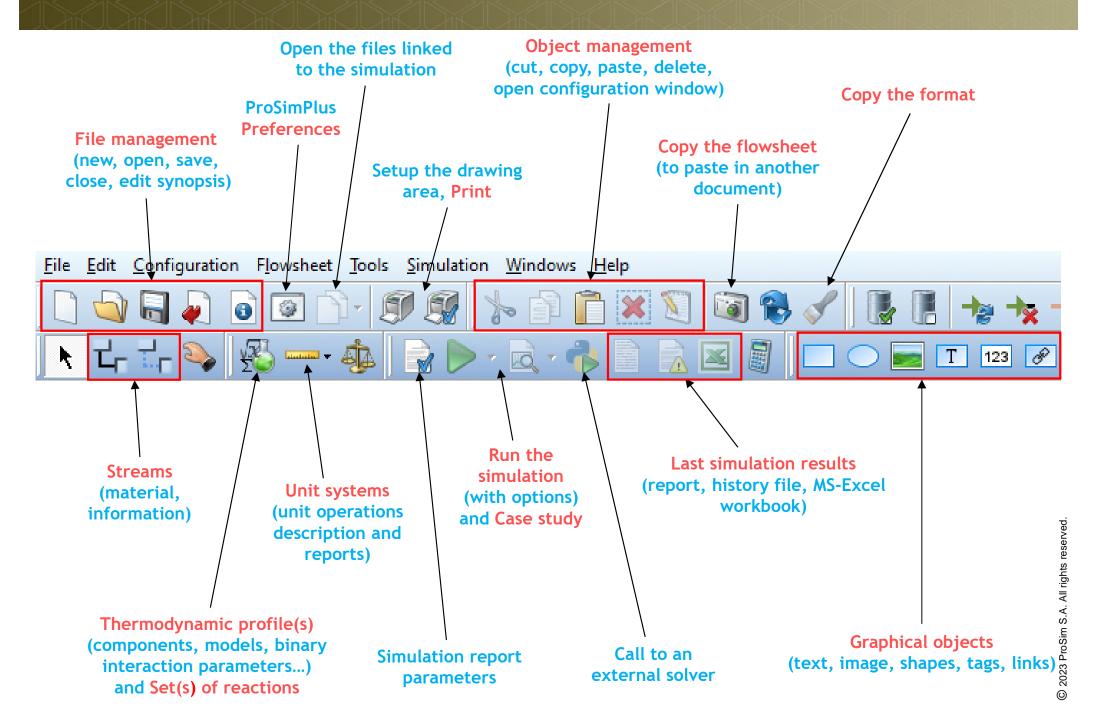
#### Introduction

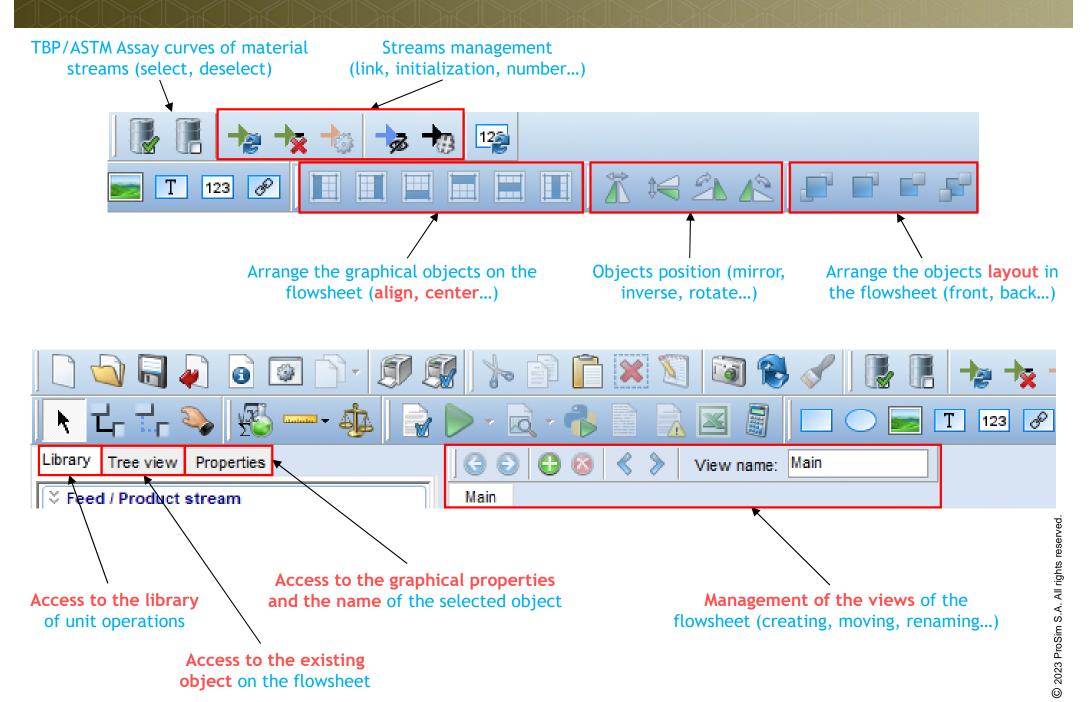
This document presents a general overview of ProSec, ProSim's CAPE-OPEN compliant unit operation dedicated to the simulation of brazed plate-fin heat exchangers. In this document, ProSec is used in ProSimPlus, ProSim's steady state simulation software.

This step by step guide describes the different functions that are used to build a simulation of a brazed plate-fin heat exchanger with ProSec. It is based on a simple heat exchanger with two fluids.









Unit operations library, tree view or properties

Beside the Library View, which presents the unit operations available in ProSimPlus within categories, the Tree View lists the items (streams and unit operations) used in the flowsheet. Selecting one (or several with the Ctrl button) item in the list selects the corresponding item in the flowsheet. Double clicking on the item in the list opens its configuration window.

The Properties tabs allows to modify the graphical aspect of any selceted items of the flowsheet.

Library Tree view Properties	Library Tree view Properties		Library Tree view Properties
∛ Feed / Outlet	Name	Initia	Information
Flashes and Decanters	CO-PROSEC		
☆ Heat exchangers	Hot inlet		Name 1
Cooler/Heater	Cold stream		Description
G Cooler/Heater	Hot outlet		
	Hot side stream		Stream
Simple heat exchanger	Cold outlet		
(D) commentation to a second	1		Start arrow
Generalized heat exchanger	<b>→</b> 2		Middle arrow
	→ 3		End arrow
MHX MHX	→ 4 → 5		
CO-ProSec	5		Cisplay a label
00-10360			Line / Outline
CO-ProSim PHE			
			C Enabled
× Pressure changers			Color
X Mixers / Splitters / Separators			

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#### Library view

#### Tree view

#### Properties

#### Building the flowsheet

- The steps are the following:
  - ✓ Step 1: Select your components
  - ✓ Step 2: Select your thermodynamic model
  - ✓ Step 3: Create your flowsheet
  - ✓ Step 4: Run the simulation
  - ✓ Step 5: Reports generated
  - ✓ Step 6: Analyze the results from the flowsheet
  - ✓ Step 7: Share the simulation

### Step 1: Select your components

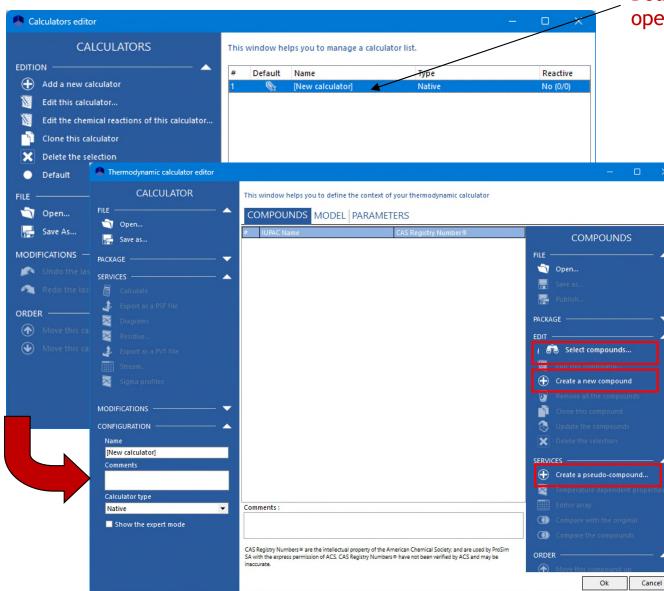
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Library Tree view Properties	🔕 < 📎 View name: Main		thermodynam	ic models.	
Feed / Outlet Main					
Flashes and Decanters					
V Heat exchangers					
Yressure changers     Mixers / Splitters / Separators					
✓ Initice of Spin actions ✓ Optimization & Design specifikations	Calculators editor			- • ×	
i Tools	CALCULATORS	This window helps you to manage	a calculator list		
Vser defined unit operations		This which where you to manage			
Subflowsheet		# Default Name	Туре	Reactive	
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1	Move this calculator down	Comments:			
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				Ok Cancel	
		-			
					- You can use severa

Click on the Thermodynamics and Compounds icon to open the calculators editor.

You can use several calculators in the same flowsheet.

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#### Step 1: Select your components



## Double click on the "New calculator" to open the calculator environment window.

To <u>search</u> for a component in one of the databases, click on "Select compounds"

To <u>create</u> a component "from scratch" with the properties that you have, click on "Create a new compound"

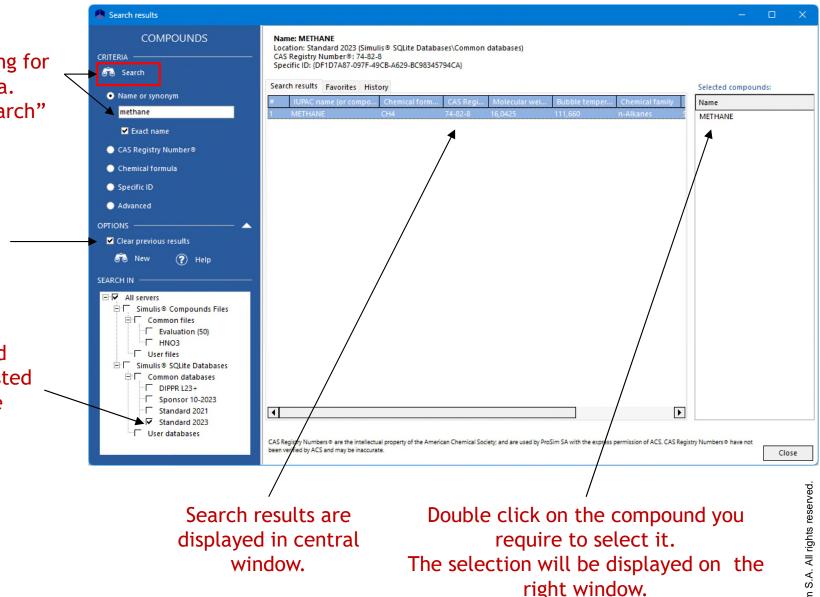
To <u>create pseudo compounds</u>, without lights ends, click on "Create a pseudo-compound"

#### **Step 1: Select your components**

Enter the name of the compound you are looking for or select another criteria. Once entered, press "Search"

Check this box to clear previous results

The databases registered on your computer are listed here. Select the last one (in date)



Repeat the operation to select all the components that you need. For this simulation you will need methane and ethane.

## Step 2: Select your thermodynamic model

Once all components are selected, close the component search window to return to the Calculator edition environment.

Click on the "Model" tab to enter the thermodynamic selection environment.

Select an appropriate thermodynamic model using the pull down menu. Here we use Peng-Robinson.

Thermodynamic calculator editor				- 0	×
	This window helps you to define the COMPOUNDS MODEL BI		lator		
Open     Save as  PACKAGE	Name Category Profile Approach type Equation of state Alpha function Mixing rules Activity coefficient model Pure liquid fugacity standard state Liquid molar volume Transport properties Enthalpy calculation User-defined thermodynamic model	Peng-Robinson (PR) All the profiles Peng-Robinson (PR) Using Equation of state PR Generalized Peng-Robinson (76) Standard Not defined		THERMODYNAMIC MODEL DOCUMENTATION   Thermodynamic assistant  ADDITIONAL PARAMETERS  MODEL INFORMATION  WATER-HYDROCARBON  PURE WATER	
				Ok Canc	el

When the selected thermodynamic model requires binary interaction parameters, the "Binaries" tab appears.

## Step 2: Select your thermodynamic model

#### By default, for a new calculator, the available binaries are automatically loaded.

Thermodynamic calculator editor		– 🗆 X
Thermodynamic calculator editor     CALCULATOR     FILE   Image: Constraint of the stream of the strea	This window helps you to define the context of your thermodynamic calculator         COMPOUNDS       MODEL       BINARIES       PARAMETERS         These parameters correspond to the general values and are used if the user has not provided each option in the thermodynamic profile)       Binaries view: • Grid • Matrix         Binaries view: • Grid • Matrix       • Matrix         Formulation : Kij = Kij0 + KijT*T         Compound Compound Kij0 KijT         METHANE       ETHANE	specific parameters (buttons to the right of BINARIES ACTIONS Import binaries Clear all binaries Estimate binaries Save the binaries
Stream Sigma profiles MODIFICATIONS   CONFIGURATION  Name [New calculator] Comments  Calculator type Native  Show the expert mode	Not supplied     Supplied     Imported     Estimated     Error       Comments :	OPTIONS ▲ Unit ■ parameters will be ignored ✓ parameters are automaticcaly loaded
		Ok Cancel

Now that your thermodynamic profile is completed click on "OK" to validate and close the window.

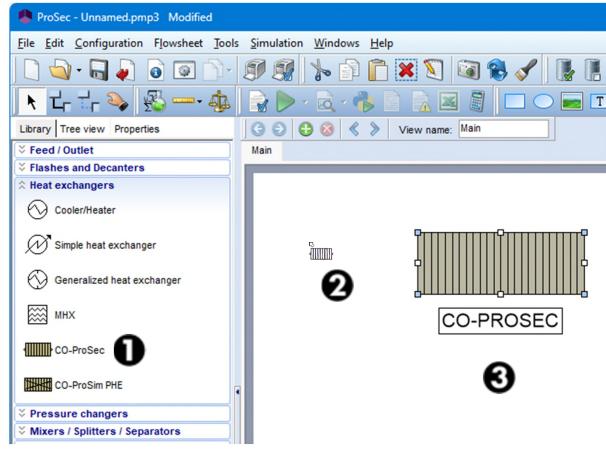
#### Step 3: Create the flowsheet

- A. ProSec unit operation
- B. Feed (inlet) and product (outlet)
- C. Connect all the unit operations with streams

1- Click on "CO-ProSec" icon in the library category "Heat exchangers" to select ProSec unit operation.

2- Move the mouse onto the drawing sheet to where you want to place the unit operation.

3- Click again, to release the unit.





A comprehensive set of features allows you resize, rotate, reposition, align, etc. the element on the drawing area.

U

To configure the ProSec unit operations:

- 1. Double-click on its icon on the flowsheet or select "Edit..." in the contextual menu
- 2. Press the "Parameters" tab
- 3. Press the "Edit..." button

	🐥 ProSec - Unnamed.pmp3 Modifie	ed	
	<u>File Edit Configuration Flowsheet</u>	t <u>T</u> ools <u>S</u> imulation <u>W</u> indows <u>H</u> elp	
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' in	Library Tree view Properties	G O C C C C C C C C C C C C C C C C C C	
	Feed / Outlet	Main	
	Flashes and Decanters		
	☆ Heat exchangers		
	Cooler/Heater		
	Simple heat exchanger		TTTTT
🔹 CO-ProSec	c (\$XTMO)		
Name: CO-PRO	SEC	Edit	
Desc: Brazed p	plate-fin heat-exchanger	Calcula	tors 🕨
	Parameters Reports Scripts Report Streams No	otes Advanced parameters	► Inhal
Specification	is management		
Edit	Open the edition window of the unit operation in order to visualize or to modify its parameters.	Thermodynamics Scriptle Move to	
Details	Visualize the registered details of the unit operation on your computer.	Output streams calculators     Image: Bring to       Output streams     Image: Bring to       Output streams     Image: Bring to	
Parameters	Open the edition window of the unit operation supplied by Simulis.	Default calculator  V Select for each stream	
Validate	Manually start the validation of the unit operation.	Stream Model	
Reports	Visualize the reports supplied by the unit operation.		
	ttons correspond to actions which are not available h are not implemented by the unit operation.		
		<u>O</u> K <u>C</u> ancel	

- "Parameters" tab
  - ✓ Fill in the general characteristics of the heat exchanger as shown on the figure below

•	CO-PROSEC - CO-ProSec -	
HOME		
Import Export Export Synopsis Presult parameters Presult parameters Presult parameters Presult parameters	Conversion tool	ita and resi
File Document	Units	^
PARAMETERS CATALYSTS   STREAMS   FINS   REFERENCE LAYERS   II		
Body	Dimensions	
Body number  1  Orientation (α)  Vertical: α = 90°  Other  0°  Fin database  -> 2002  Material	Used width (Wu) 589 mm Thickness of the side bars (Elat) 14,3 mm Thickness of the end bars (Eext) 27 mm Thickness of the separation plates (Esep) 1,8 mm Thickness of the dosing plates (Edo) 1,8 mm W	Edo

Change the default selection for the orientation and the fin database

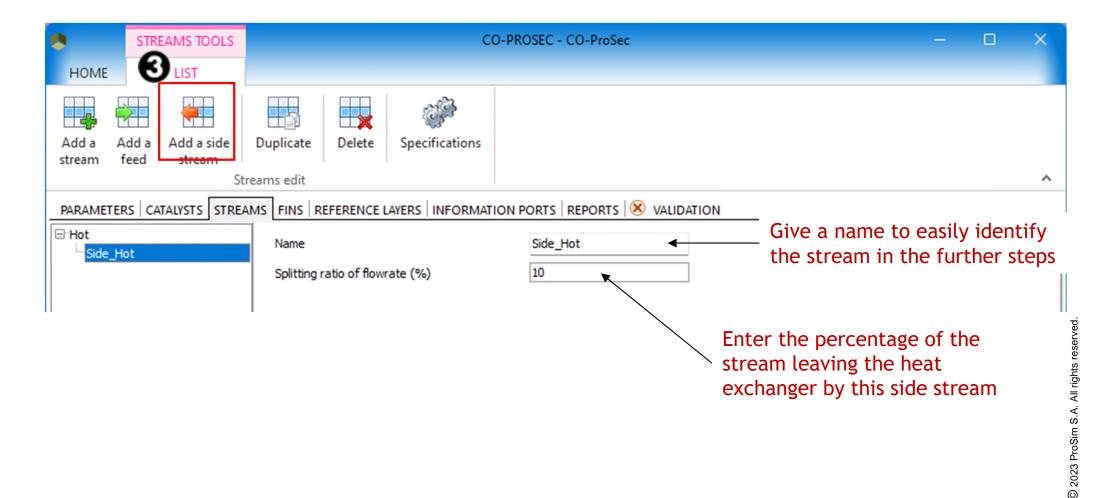
- "Streams" tab
  - Describe the two streams of the heat exchanger: a hot stream with a side stream and a cold stream
  - 1. Click on "Add a stream" to add the hot stream

		STR	EAMS TOOLS			C	D-PROSEC - CO-ProSec 📃 🗆	×					
	HOME		LIST										
0	Add a stream	Add a feed	Add a side stream	Duplicate	uplicate Delete Specifications Management of the stream list								
F	PARAMETERS CATALYSTS STREAMS FINS REFERENCE LAYERS INFORMATION PORTS REPORTS & VALIDATION												
i		ERS   CA	TALYSTS STRE		REFERENCE								
	Hot			Name			✓ Hot Specification						
							Cross flow						
							Continuous thermodynamic						
							Reactive						
							A catalyst is taken into account	/					
				Enthalp	c factor		0 kg/s 💌						
				Directio	n of circulatio	n	From top to bottom $\sim$						
				Oversiz	ng ratio on fl	owrate (%)	0						
				Fouling	actor		0 W/m2/K						

- "Streams" tab
  - 2. Describe the stream "Hot" characteristics

PARAMETERS CATALYSTS STREAM	MS	FINS   REFERENCE LAYERS   INFORMATION PORTS   REP	Give a name and select	
<sup></sup> Hot		Name dRed ~	Hot a color to easily	
			Cross flow identify the stream in the further steps	
			Continuous thermodynamic	
			Reactive	
			A catalyst is taken into account	
		Enthalpic factor	0 kg/s	
		Direction of circulation	From top to bottom $\sim$	
		Oversizing ratio on flowrate (%)	• Change the default	
	h	Fouling factor	<sup>0</sup> W/m2/K correlation for the heat	
	Ш	Correlation used to calculate the exchange coefficient	HTES 85	
	Ш	Threshold where the mixture is dealt as pure (%)	<sup>99,99</sup> transfer coefficient	
	Ш	Generation of physico-chemical properties	tabulated Calculation	
	۲	Supercritical fluid	Calculation phase	
	Ш	Number of tabulated points -		
	Ш	Extrapolation (DT)	5 K 🔽	201
	Ш	Diphasic zone		2000
	۲	Minimum number of diphasic points -		-+0
		Option of diphasic tabulation	Difference of enthalpy $\sim$	2:2
		Pressure drop is taken into account		<
		Initial pressure drop	0 bar	6
		Maximum pressure drop	0,2 bar	0
		Safety margin (DT)	5 K	1 000
		Output temperature (UA calculation)	0 К	0

- "Streams" tab
  - 3. Click on "Add a side stream" to add the stream "Hot" side stream
  - 4. Fill in the characteristics of this side stream



- "Streams" tab
  - 5. Click on "Add a stream" to add the cold stream
  - 6. Describe the stream "Cold" characteristics

_					
	Add a Add a Add a side stream	Duplicate Delete Specifications			
	Str	eams edit			^
	PARAMETERS CATALYSTS STREA	MS FINS REFERENCE LAYERS INFORMATION PORTS RE	PORTS		Give a name to easily identify
Ī	🖃 Hot	Name dBlue ~	Cold	Specification	
	Side_Hot		Cross flow		the stream in the further steps
	Cold		Continuous thermodynamic		
			Reactive		
			A catalyst is taken into account		Change the default direction of
		Enthalpic factor			Change the default direction of
			0 kg/s 🔻		circulation and the default
		Direction of circulation	From bottom to top		correlation for the heat transfer
		Oversizing ratio on flowrate (%)	0		
		Fouling factor	0 W/m2/K		coefficient calculation
		Correlation used to calculate the exchange coefficient	HTFS 85 V	0 W/m2/K	
		Threshold where the mixture is dealt as pure (%)	99,99		
		Generation of physico-chemical properties	tabulated		
		Supercritical fluid	Calculation phase	Automatic	✓
		Number of tabulated points	-	+	
		Extrapolation (DT)	5 K 👻		
		Diphasic zone			
		Minimum number of diphasic points	-	+	
		Option of diphasic tabulation	Difference of enthalpy $\sim$		
		Pressure drop is taken into account			
		Initial pressure drop	0 bar		
		Maximum pressure drop	0,2 bar		
		Safety margin (DT)	5 K		
		Output temperature (UA calculation)	0 К		

- "Fins" tab
  - ✓ Describe the two fins used in the heat exchanger
  - Fin #1 (for heat exchange zones) is a user-defined, for which performance data are given
  - Fin #2 (for distributors) is a user-defined, for which performance data are calculated from correlations
  - 1. Click on "Add a fin"

	FINS	TOOLS				CO	-PROSEC - C	CO-ProSec	
HOME	1	LIST							
Add a fin	Duplicat		Move up selected		down	Delete the selected fin	Impoi user fin	Aanagement	of the fin list
PARAME	TERS	TALYSTS	STREAMS	FINS REFERE	NCE LAYER			REPORTS 😣 VALIDATI	ON
Name		Reference	e #	Origin		Calculation mo	de		
		0		Standard datab	ase 💌	From geometry	etry		
						OPerformanc	e data provid	led	

- "Fins" tab
  - ✓ Fin #1 description
  - 2. Give a name
  - 3. Select the "Origin" (Standard database or User)
  - 4. Give a reference number
  - 5. Fill in the characteristics

Name Reference #	Origin	Calculation mode					
Fin #1 1001	User	From geometry	y				
5 6	6	O Performance d	lata provided				<u> </u>
6 0	0	Туре	Right fin	~		7777	$\mathcal{A}$
		Height	7,13 mm	-	e	p	
		Thickness	0,4 mm	-			
		Fins number per me	ter 673,2				
		Perforation porosity	(%) 0				
		Serration length	0 mm	-			
		Metal section correc	ction 0			-	Colburn coefficier
		Global efficiency	1		46	0,98874	0,06258
		Fin efficiency is	taken into account		122	0,39326	0,04122
		Duct diameter	0 mm		200	0,26355	0,03266
					538	0,14066	0,02048
		Duct absolute rugos	-	· · · · ·	881	0,113	0,01643
		Duct wet perimeter	0 mm	•	1442	0,09665	0,01337
		Duct section	0 m2	•	2363	0,08753	0,01106
		Ducts number per m	neter 0		6338	0,0818	0,00797
		HTC correlations:			17003	0,08171	0,00604
		User code (VBSc	ript) on the whole area		45614	0,0726	0,00462
		Laminar flow	In-house correlation	~			
		Turbulent flow	In-house correlation	~			
		Friction factor corre	lations:				
		User code (VBSc	ript) on the whole area				
		Laminar flow	In-house correlation	~			
		Turbulent flow	In-house correlation				

"Fins" tab

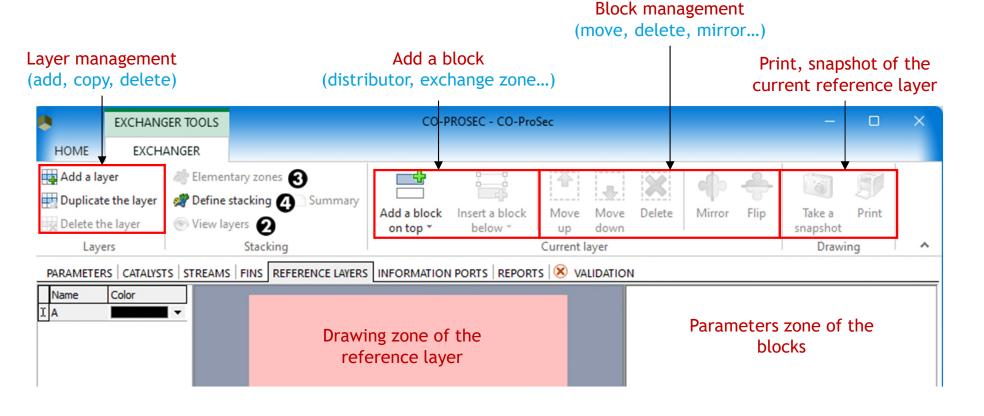
<ul> <li>Fin #2 description</li> </ul>	
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	252116			X III XX III			
	: L	IST					
Add a fin	Duplicate				mport a user fin		
PARAME	TERS CAT	ALYSTS STREAMS	FINS REFERENCE LAY	ERS INFORMATION P		ORTS 😣 VAL	DATION
Name	F	Reference #	Origin	Calculation mode			
Fin #1	1	.001	User 🔹	O From geometry			
Fin #2	7	7844	User 🔽	O Performance da	ta provided		
2	•	0	€	Туре		Right fin	~
		-	-	Height		7,13 mm	-
				Thickness		0,4 mm	-
				Fins number per met	er	200	
				Perforation porosity	(%)	0	
				Serration length		0 mm	-
				Metal section correct	tion	0	
				Global efficiency		1	
				Fin efficiency is ta	aken into acco	ount	
				Duct diameter		0 mm	-
				Duct absolute rugosi	ty	0 mm	-
datab	base c	or User)		Duct wet perimeter		0 mm	-
		/		Duct section		0 m2	-
				Ducts number per me	eter	0	
				HTC correlations:			
				User code (VBScri	ipt) on the wh	nole area	
				Laminar flow	In-house co	rrelation	$\sim$
				Turbulent flow	In-house co	rrelation	$\sim$
				Friction factor correla	ations:		
				User code (VBScri	ipt) on the wł	nole area	
				Laminar flow	In-house co	rrelation	~
				Turbulent flow	In-house co	rrelation	~

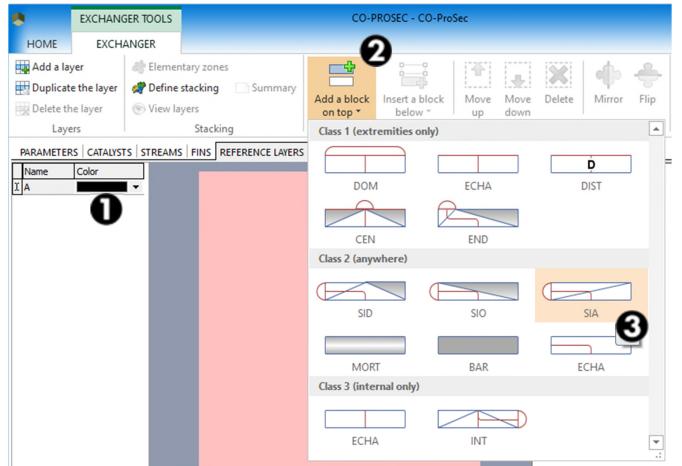
- 1. Click on "Add a fin"
- 2. Give a name
- 3. Select the "Origin" (Standard database or User)
- 4. Select the reference "7844"
- 5. Fill in the characteristics

#### "Reference layer" tab

- $\checkmark$  Describe the reference layer, the meshing and the stacking
- 1. Describe the reference layers
- 2. Visualize the layers
- 3. Adjust the number of discretization cells
- 4. Define the stacking

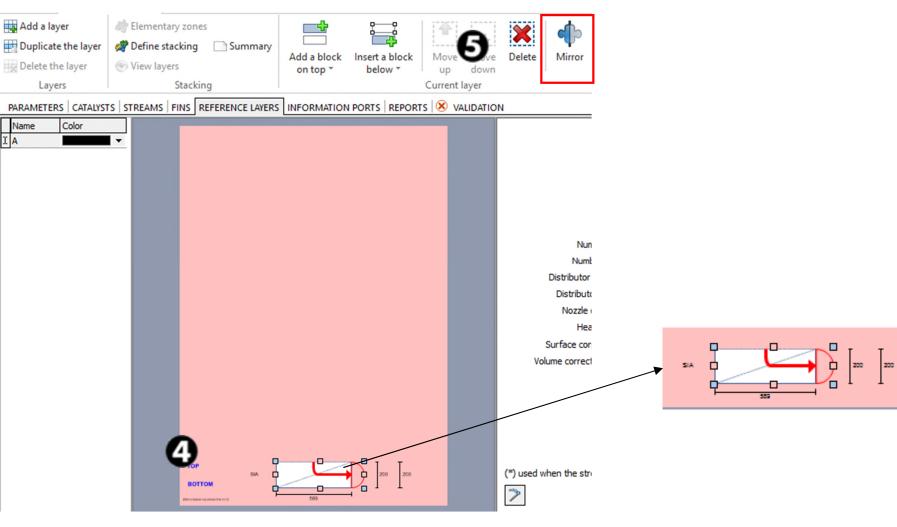


- "Reference layer" tab
  - ✓ Describe the reference layer "A" (hot stream reference layer)
  - 1. Select a color to easily identify this layer in the stacking description
  - 2. Click on "Add a block on top"
  - 3. Select the first block to add a "SIA" distributor

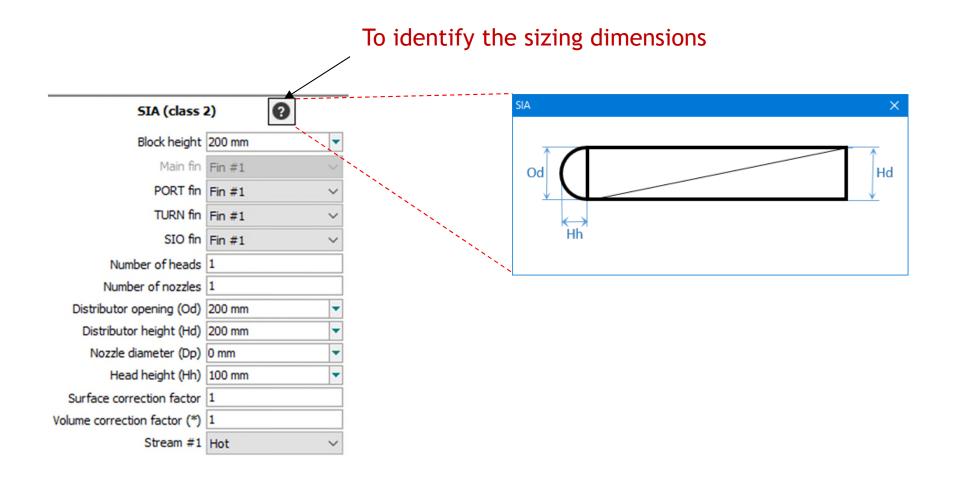


#### "Reference layer" tab

- 4. Click on the block to select it
- 5. Click on "Mirror" to change the position of its head



- "Reference layer" tab
  - 6. Fill in its parameters



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- "Reference layer" tab
  - 7. Click on "Add a block on top" and select a heat exchange zone "ECHA"
  - 8. Select this block and enter its parameters

	_		
6		ECHA (class	3)
1	<b>* 🙀 👔 🙀 🔶 🚳 .</b>	Block height	612 mm 🔻
	Insert a block Move Move Delete Mirror Flip Take a	Main fin	Fin #1 $\vee$
	below * up down snapshot Class 1 (extremities only)	PORT fin	Fin #1 $\sim$
		TURN fin	Fin #1 $\sim$
i		SIO fin	Fin #1 $\sim$
	DOM ECHA DIST	Number of heads	1
		Number of nozzles	1
	CEN END	Distributor opening (Od)	0 mm
	Class 2 (anywhere)	Distributor height (Hd)	0 mm
		Nozzle diameter (Dp)	0 mm
		Head height (Hh)	0 mm
	SID SIO SIA	Surface correction factor	1
		Volume correction factor (*)	1
	MORT BAR ECHA	Stream #1	Hot $\checkmark$
	Class 3 (internal only)		
	ECHA INT	ECHA C 612 TZ6 (*) used when the stream is reactive	
		Update	visual Restore

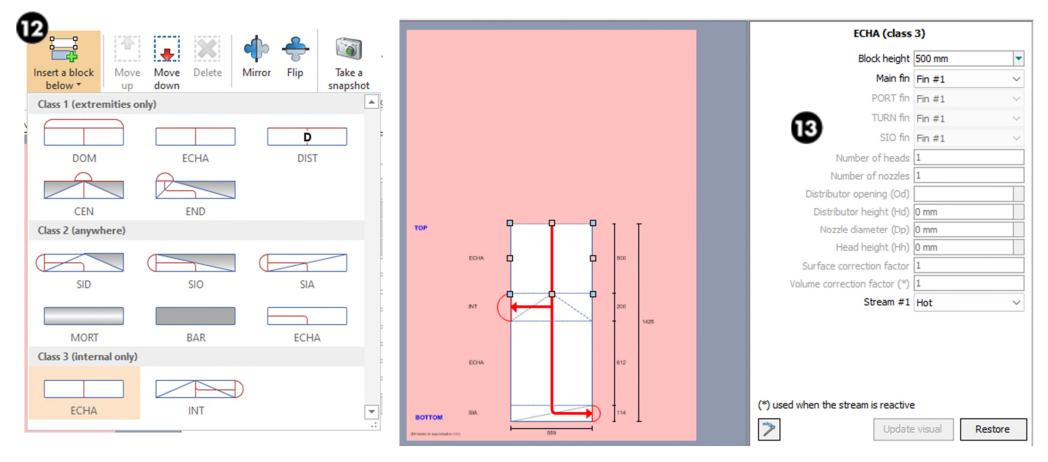
"Reference layer" tab 

- 9. Click on "Add a block on top" and select an "INT" distributor
- 10. Click on "Mirror" to change the position of its head
- 11. Select this block and enter its parameters

9 🕂 🗼 🗶 🔶	ry zones acking Summary rs Stacking Stacking	ete Mirror Flip Take a Print snapshot Drawing ^
Add a block Insert a block Move Move Delete Mirror Flip	REFERENCE LAYERS INFORMATION PORTS REPORTS X VALIDATION	INT (class 3)
Class 1 (extremities only)		Block height 200 mm
		Main fin #1
P		
DOM ECHA DIST		TURN fin #2 ~
		SIO fin #2 V
		Number of heads 1
CEN END		Number of nozzles 1
Class 2 (anywhere)		Distributor opening (Od) 200 mm
		Distributor height (Hd) 200 mm
		Nozzle diameter (Dp) 0 mm
SID SIO SIA		Head height (Hh) 100 mm
		Surface correction factor 1
		Volume correction factor (*) 1
MORT BAR ECHA		Stream #1 Hot 🗸
Class 3 (internal only)		
		Freed
ECHA INT	•	Sidestream Side_Hot ~
		Update visual Restore

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- "Reference layer" tab
  - 12. Click on "Add a block on top" and select a heat exchange zone "ECHA"
  - 13. Select this block and enter its parameters



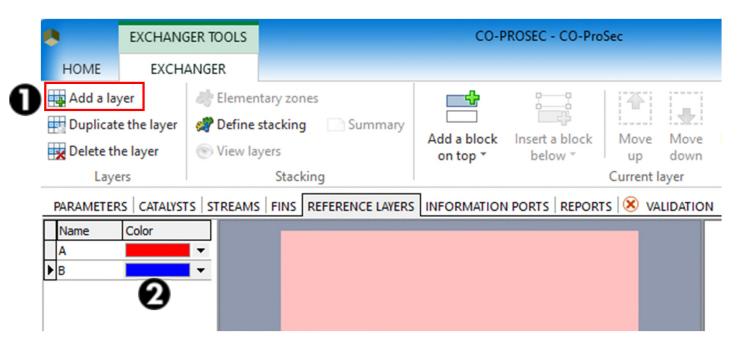
- "Reference layer" tab
  - 14. Click on "Add a block on top" and select an "SID" distributor
  - 15. Click on "Mirror" to change the position of its head
  - 16. Select this block and enter its parameters

Add a block on top	Insert a block below *	Move	Move down	<b>X</b> Delete	d Mirror	Fli
Class 1 (extr	emities only)					[
DOM		ECHA			<b>D</b> IST	]
CEN		END				
Class 2 (anyw	vhere)					
SID		SIO			SIA	]
MOR		BAR			ECHA	]
Class 3 (inter	rnal only)					
ECHA		INT				

king Summary Add a block Insert a block on top * Ibelow Current layer REFERENCE LAYERS INFORMATION PORTS REPORTS VALIDATION Tore so top to the source of th	ei its pai	ameter	3		ิด	3		
REFERENCE LAYERS INFORMATION PORTS REPORTS VALIDATION SID (class 2) Block height 114 mm Main fin Fin #1 PORT fin Fin #2 TURN fin Fin #2 TURN fin Fin #2 SIO fin Fin #2 Number of neades 1 Number of neades 1 Distributor opening (Od) 114 mm Distributor height (Hd) 114 mm Nozzle diameter (Dp) 0 mm Head height (Hb) 57 mm Surface correction factor (*) 1 Stream #1 Hot	y zones cking 📄 Summary s Stacking		below *	up down		Mirror Flip	snapshot	rint
SID (class 2)       Block height         Block height       114 mm         Main fin       Fin #1         PORT fin       Fin #2         TURN fin       Fin #2         SIO fin       Fin #2         Number of heads       1         Number of nozzles       1         Distributor opening (Od)       114 mm         Nozzle diameter (Dp)       0 mm         Head height (Hd)       114 mm         Nozzle diameter (Dp)       0 mm         Head height (Hd)       57 mm         Surface correction factor (*)       1         Stream #1       Hot	_	NFORMATION PO			N			
TOP       SD       Image: state of the state of				_		SID (clas	c 2)	0
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(*) used when the stream is reactive	ECHA		612					
(*) used when the stream is reactive								
					(*) used v	when the stream is reac	tive	
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#### "Reference layer" tab

- ✓ Describe the reference layer "B" (cold stream reference layer)
- 1. Click on "Add a layer" to add a new reference layer
- 2. Select a color to easily identify this layer in stacking description

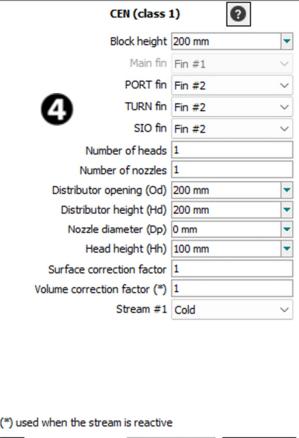


- "Reference layer" tab
  - 3. Click on "Add a block on top" and select a "CEN" distributor

550

4. Select this block and enter its parameters

Add a block Insert a b		Delete Mirror Flip
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Class 2 (anywhere)		2
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MORT Class 3 (internal only)	BAR	ECHA
		ž
ECHA	INT	T I
		<b>ا</b>



Update visual

Restore

- "Reference layer" tab
  - 5. Click on "Add a block on top" and select a heat exchange zone "ECHA"
  - 6. Select this block and enter its parameters

		ECHA (class 3)
6 📑 🚺 🖡 💥 💠 🔶 🚳 .		Block height 331 mm 💌
		Main fin 🛛 Fin #1 🔍
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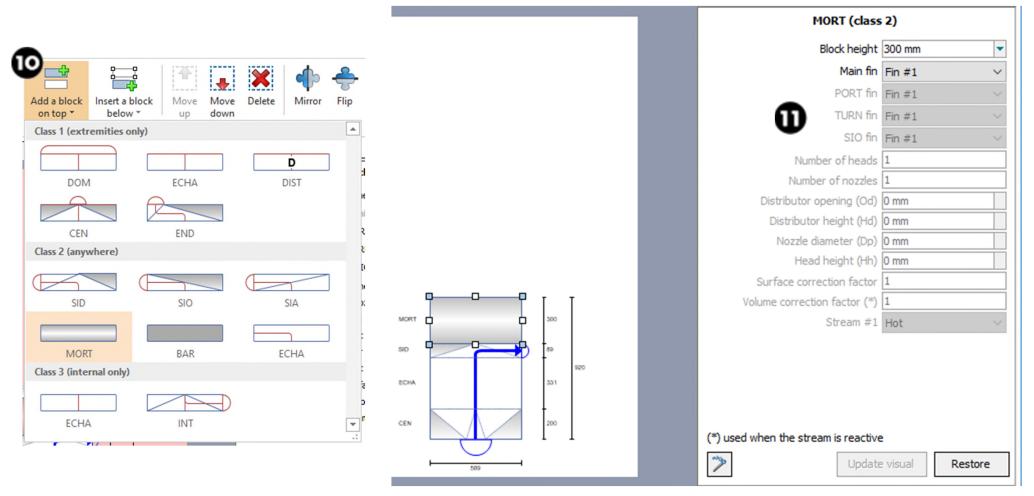
34

- "Reference layer" tab
  - 7. Click on "Add a block on top" and select a "SID" distributor
  - 8. Click on "Mirror" to change the position of its head
  - 9. Select this block and enter its parameters

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						Distributor	opening (O	d) 89 mm		-
						Distributo	or height (H	id) 89 mm		-
						Nozzle o	diameter (D	) 0 mm		-
						Hea	d height (H	lh) 44,5 mm		-
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CEN		200								
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۰	509	-			>		Upd	late visual	Resto	re

- "Reference layer" tab
  - 10. Click on "Add a block on top" and select a "MORT" zone, i.e. a zone in which no fluid flows (only conduction occurs)
  - 11. Select this block and enter its parameters



- "Reference layer" tab
  - 12. Click on "Add a block on top" and select a "SID" distributor
  - 13. Click on "Mirror" to change the position of its head
  - 14. Select this block and enter its parameters

Add a block	Insert a block	Move	- Move	X Delete	d Mirror	Fli
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Class 3 (inter	nal only)					
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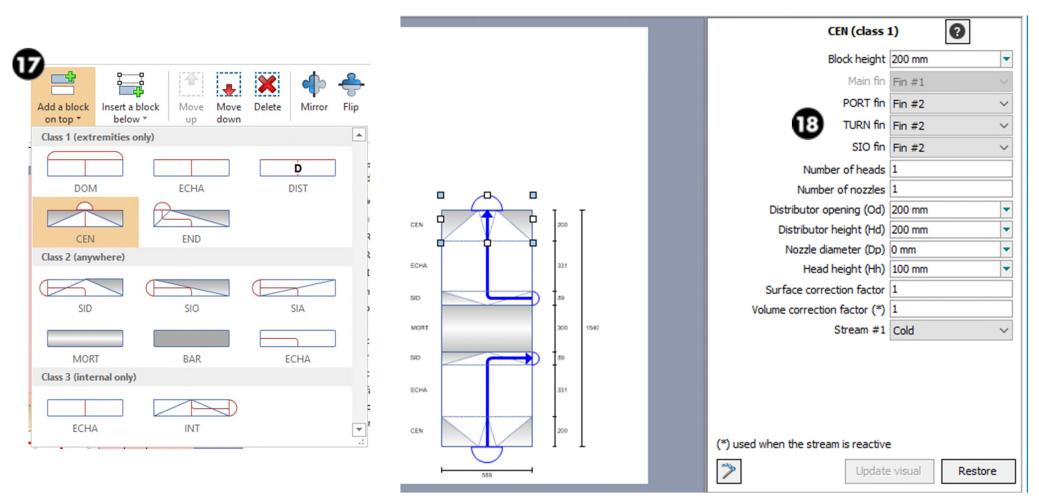
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						Nozzle	diameter (	(Dp) 0 mm	-
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SHD B	-	∎ I∞ I			1	Surface cor	rection fa	ctor 1	
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CEN		200							
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-		4			*		Un	date visual	Restore
					-				

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- "Reference layer" tab
  - 15. Click on "Add a block on top" and select a heat exchange zone "ECHA"
  - 16. Select this block and enter its parameters

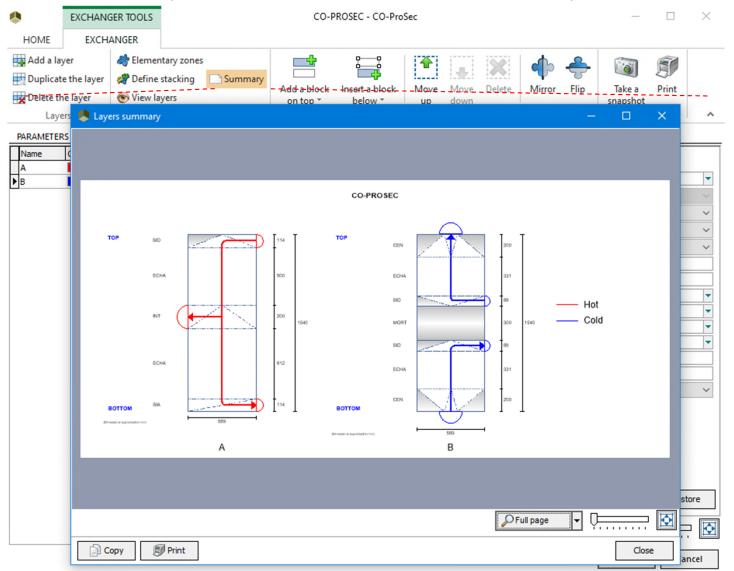
15		ECHA (class 3)
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Insert a block Move Move Delete Mirror Flip Take a		Main fin #1 V
below 🔻 up down snapshot		PORT fin #1 V
Class 1 (extremities only)		16 TURN fin #1
		SIO fin #1 V
DOM ECHA DIST		Number of heads 1
		Number of nozzles 1
		Distributor opening (Od) 0 mm
CEN END	00	Distributor height (Hd) 0 mm
Class 2 (anywhere)		Nozzle diameter (Dp) 0 mm
	ЕСНА 0 201	Head height (Hh) 0 mm
		Surface correction factor 1
SID SIO SIA		Volume correction factor (*) 1
	MORT 200 1340	Stream #1 Cold V
MORT BAR ECHA	540 59	
Class 3 (internal only)		
ECHA INT	CEN 200	(*) used when the stream is reactive
	509	Update visual     Restore

- "Reference layer" tab
  - 17. Click on "Add a block on top" and select a "CEN" distributor
  - 18. Select this block and enter its parameters



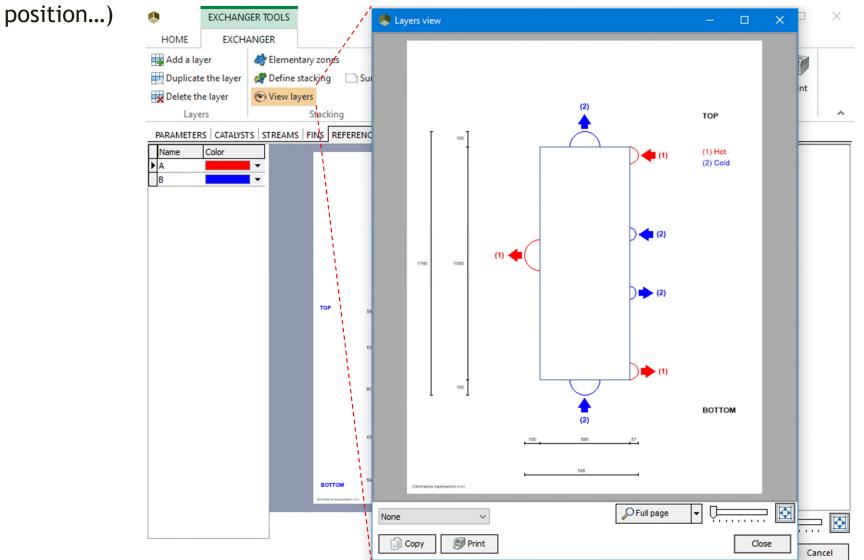
#### "Reference layer" tab

Click on "Summary" to visualize the whole reference layers

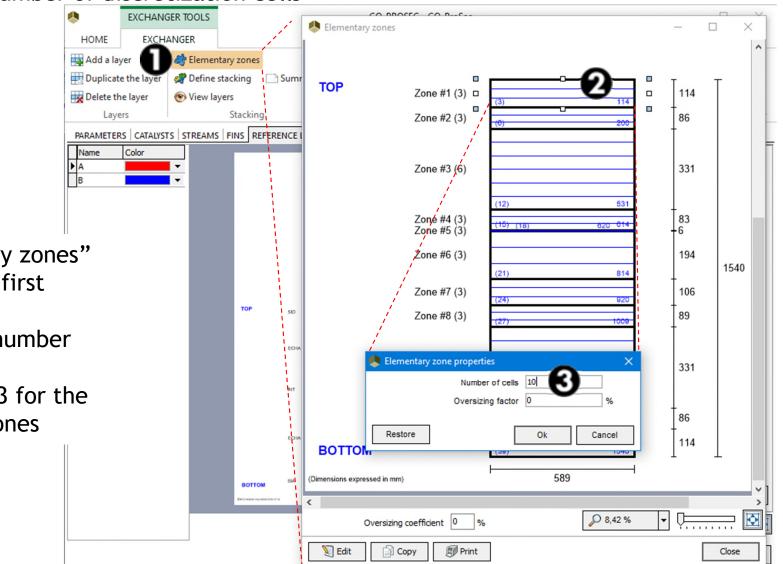


#### "Reference layer" tab

 $\checkmark$  Click on "View layers" to visualize the sketch of the heat exchanger (head

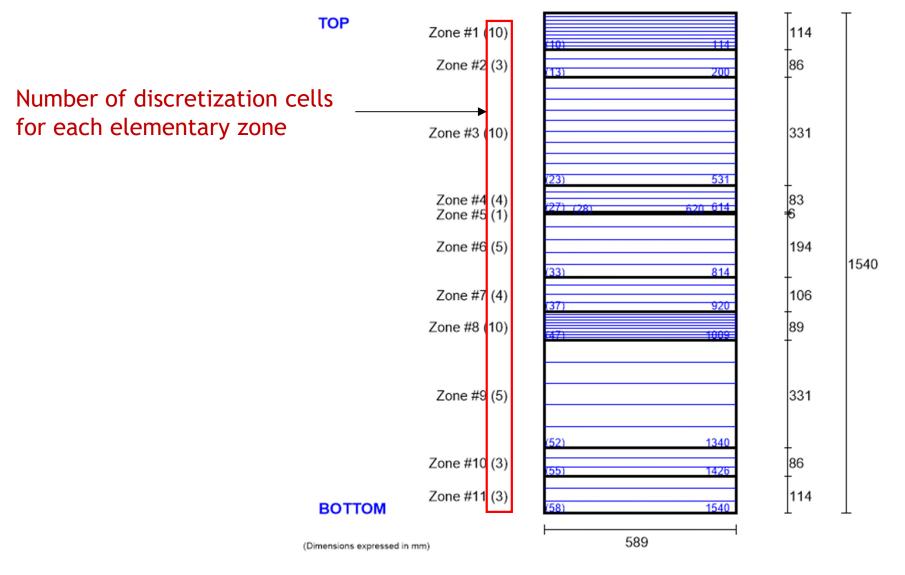


- "Reference layer" tab
  - ✓ Adjust the number of discretization cells



- 1. Click on "Elementary zones"
- 2. Double-click on the first elementary zone
- 3. Modify the default number of cells
- 4. Repeat point 2 and 3 for the other elementary zones

- "Reference layer" tab
  - $\checkmark$  Adjust the number of discretization cells

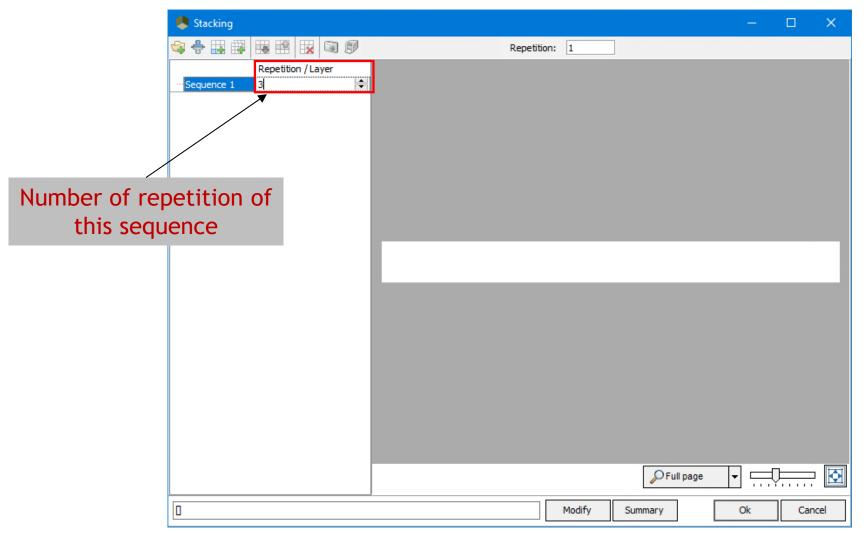


- "Reference layer" tab
  - ✓ Define the stacking: A B A B A B (6 layers)
  - 1. Click on "Add a new sequence"

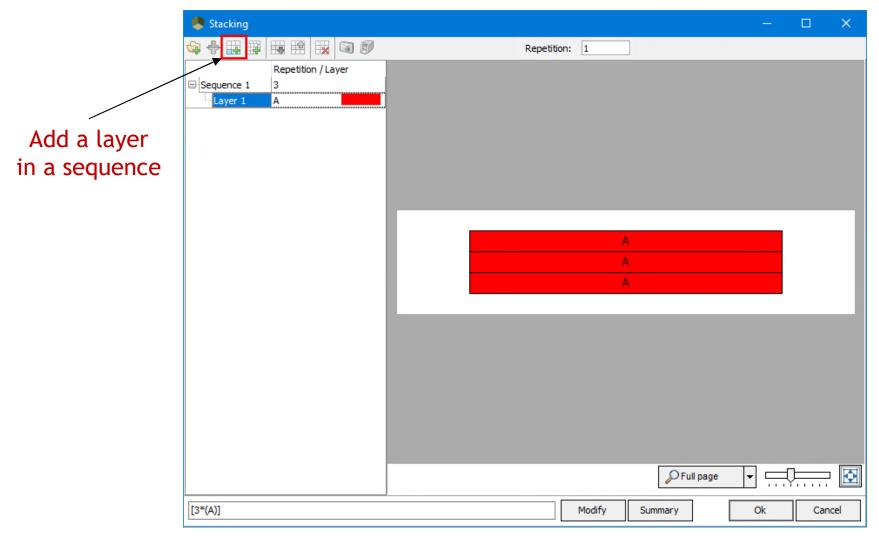
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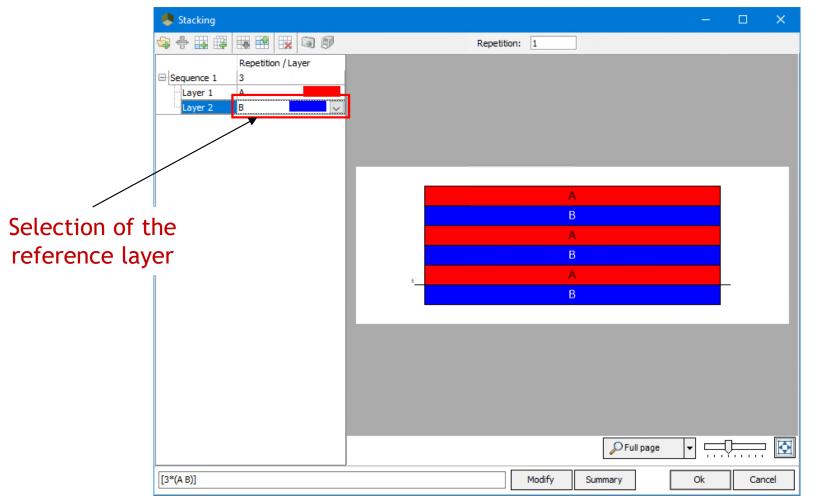
- "Reference layer" tab
  - ✓ Define the stacking: A B A B A B (6 layers)
  - 2. Specify 3 repetition for the "Sequence 1"



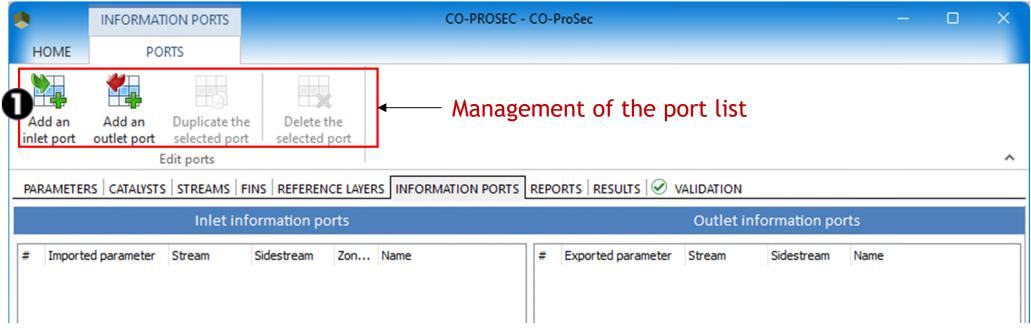
- "Reference layer" tab
  - ✓ Define the stacking: A B A B A B (6 layers)
  - 3. Click on "Add a new layer in the selected sequence"



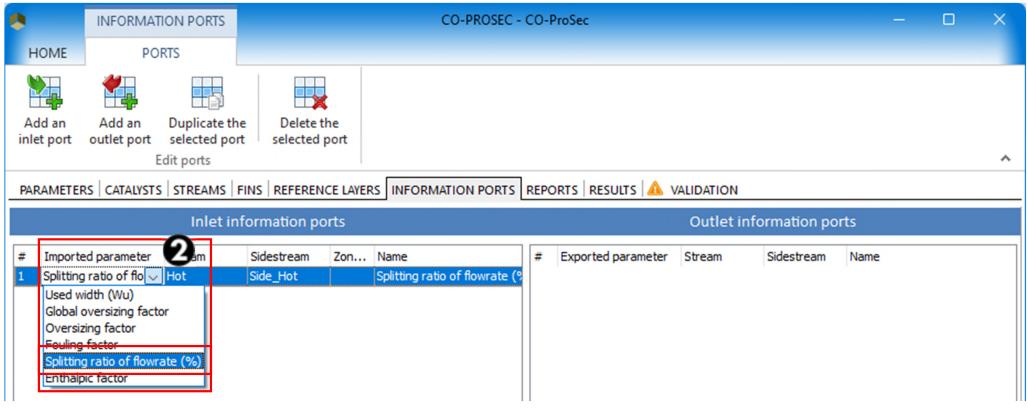
- "Reference layer" tab
  - ✓ Define the stacking: A B A B A B (6 layers)
  - 4. Click a second time on "Add a new layer in the selected sequence"
  - 5. With the menu of the "Layer 2", select the reference layer "B"



- "Information ports" tab
  - Add inlet/outlet information ports
  - 1. Click "Add an inlet port"

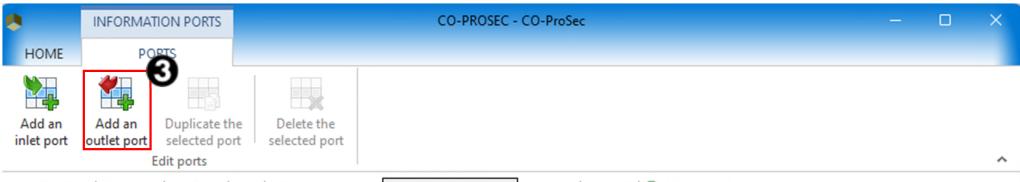


- "Information ports" tab
- 2. Select the parameter to import from another unit operation of the simulation for the inlet information port: the imported value will replace the value defined in the interface



49

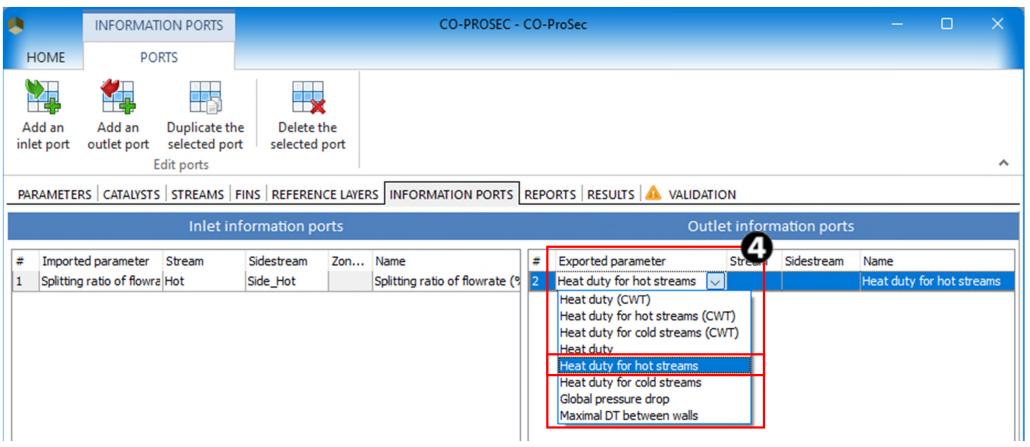
- "Information ports" tab
- 3. Click "Add an outlet port"



PARAMETERS CATALYSTS STREAMS FINS REFERENCE LAYERS INFORMATION PORTS REPORTS RESULTS VALIDATION

		Inlet in	formation po	rts			C	Outlet inform	nation ports	
# 1	Imported parameter Splitting ratio of flowra	Stream Hot	Sidestream Side_Hot		Name Splitting ratio of flowrate (%	#	Exported parameter	Stream	Sidestream	Name

- "Information ports" tab
- 4. Select the parameter to export



#### "Validation" tab

 The validation tab lists the eventual errors. At this point, errors are present due to the lack of material connections. To solve this problem, close all ProSec windows by clicking on "Ok" button.

8	CO-PROSEC - CO-ProSec	- 1	
HOME			
Import       Export         File       Synopsis         PARAMETERS       CATALYSTS    Streams Fine Fine Fine Fines F	INFORMATION PORTS REPORTS XALIDATION		^
Path	Message		
Private parameters			
Reference layers     Constant of the second se	All layers shall have the same length.		
Distributor height (Hd)	The distributor height shall be equal to the block height.		
— 🛞 в	The circuit is not valid.		
Elementary zones	Elementary zones shall be calculated.		
	Ok	(	Cancel

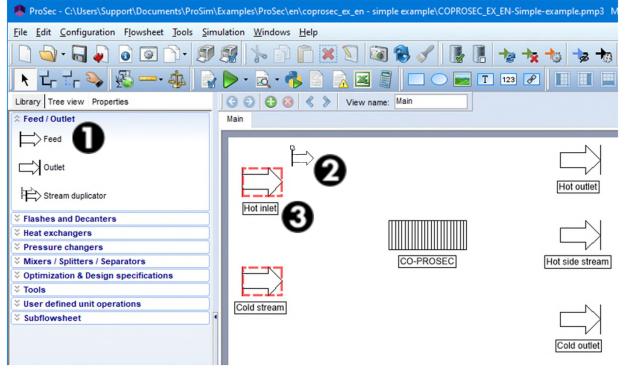
Two process feeds and three process outlets are needed for this example.

1- Click on "Process feed" icon in the library category "Feed / Product stream" to select a process feed unit operation.

2- Move the mouse onto the drawing sheet and reach the desired position.

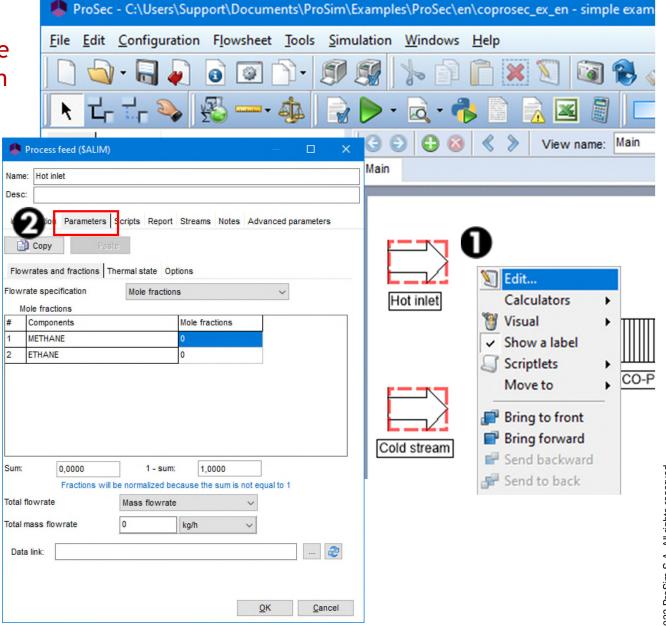
3- Click again, to release the unit.

4- Repeat to add the second process feed and the three process outlets



To configure a process feed:

- 1. Double-click on its icon on the flowsheet or select "Edit..." in the contextual menu.
- 2. Press the "Parameters" tab.



#### Hot stream inlet characteristics

•	Process feed (\$ALIM)			$ \Box$ $>$	<	Champe the default
Nam	e: Hot inlet					Change the default
Des						name (option)
l	ntification Parameters S Copy Paste			vanced parameters		
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						Fill in the mass flow rate
			<u>(</u>	<u>O</u> K <u>C</u> ancel		

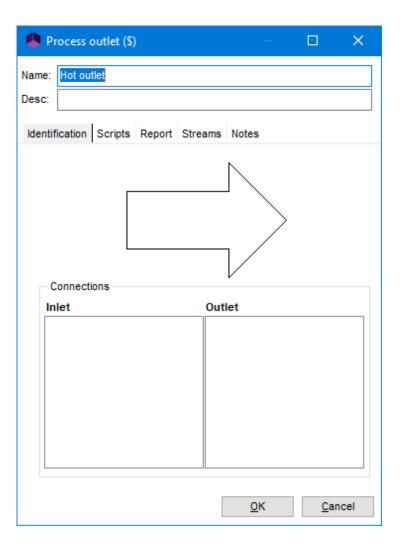
#### Hot stream inlet characteristics

Process feed (\$ALIM)			-		×
Name: Hot inlet					
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Temperature and pressure	~				
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- Cold stream inlet characteristics
  - $\checkmark$  Same characteristics as the hot stream except the temperature

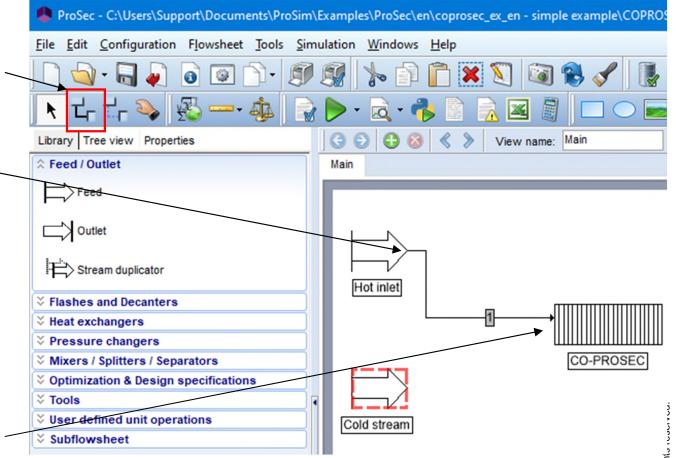
	eed (\$ALIM1)						×
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Pressure		69,4	bar	•	~		
							æ
Data link:							
Data link:							
Data link:							

- Process outlets
  - $\checkmark$  No parameters are needed for process outlets



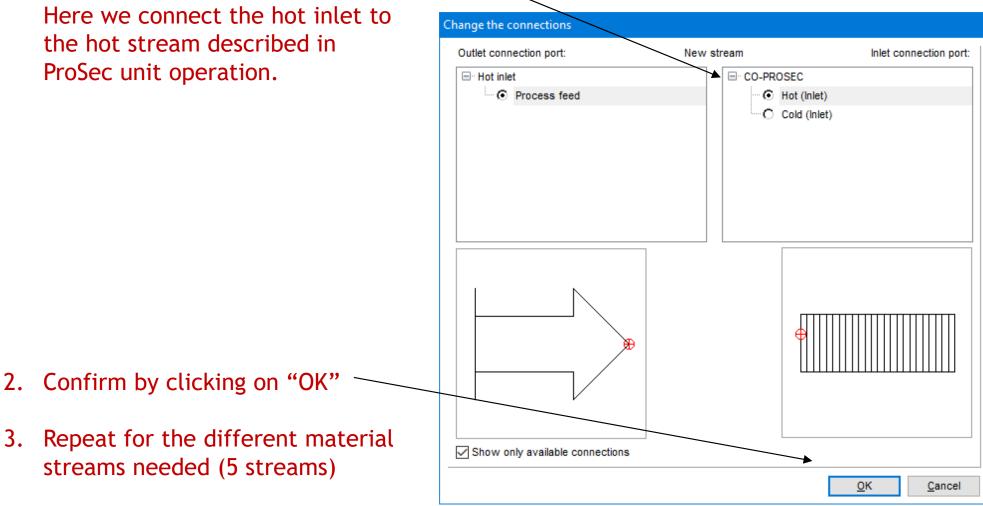
- 1. Select the "Create a material stream" icon
- 2. Select the first unit operation (source) by clicking on it

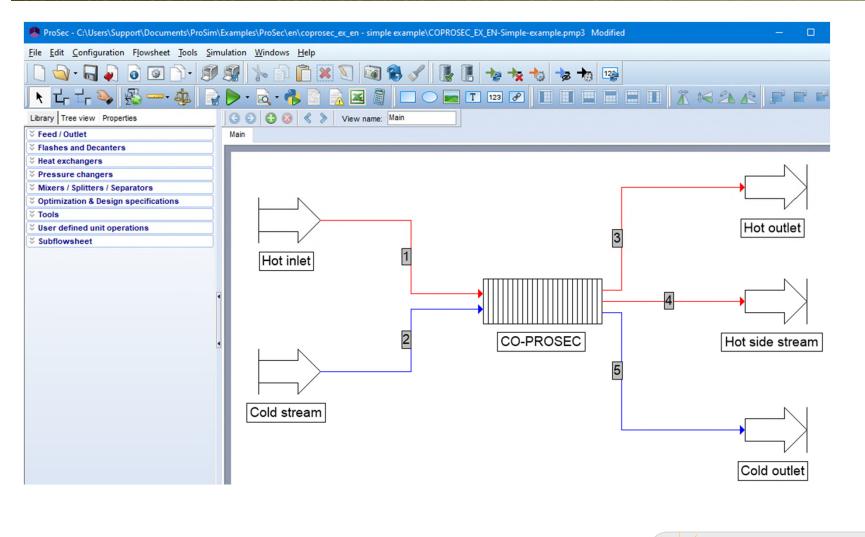
3. Select the connected unit operation (target) by clicking on it as well



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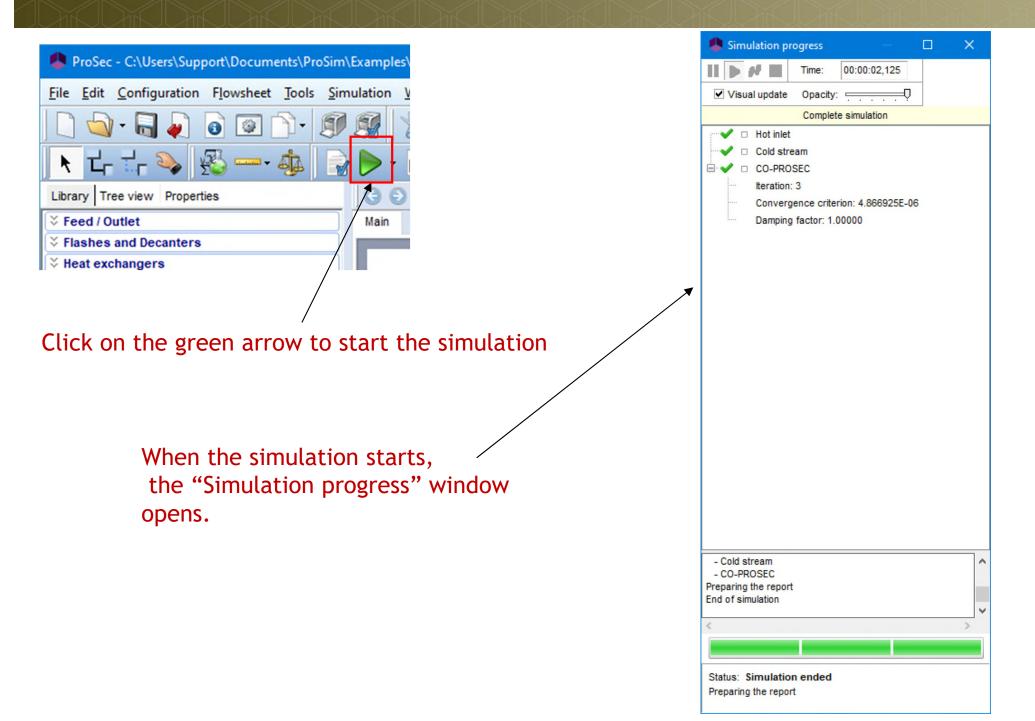
1. Select to which stream described in ProSec unit operation you want to connect the process feed. Here we connect the hot inlet to the hot stream described in ProSec unit operation.





Material streams can be colored in order to ease the reading of the flowsheet. Simply right click on the stream to access the option.

# Step 4: Running the simulation



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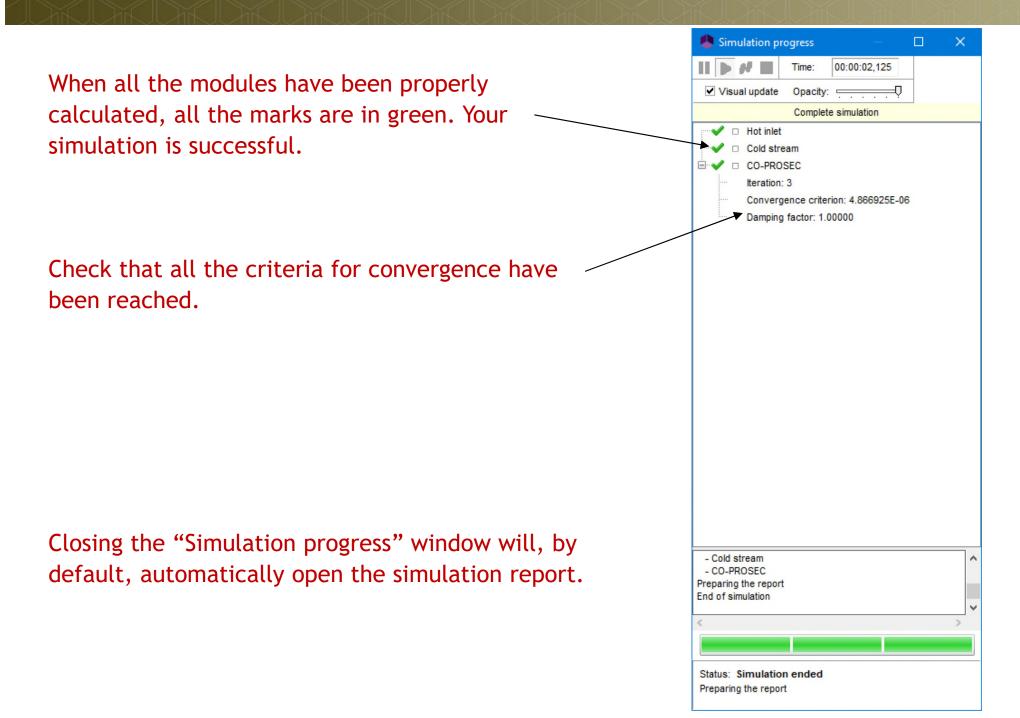
# Step 4: Running the simulation

During the calculation, different symbols and indications will appear and disappear in the "Simulation progress" window and in the drawing area.

- A green validation mark indicates that the module has been correctly calculated
- A blue arrow indicates that calculation is in progress
- A blue question mark indicates that the module has not been calculated yet
- 🎸 🔝 A red cross indicates a convergence error

Simulation progress		- 0 🛛
Image: Second	Name of the Rem.	
Reading data Checking data Receiving calculation sequence Smulation in progress		
Unit operation "Hot inlet" converged.		Pfull page 🔹 🚃 🐼

# Step 4: Running the simulation



## Step 5: Reports generated

- A. ProSec unit operation tabulated results
- B. ProSec unit operation graphical results
- C. ProSimPlus general reports

To consult the reports generated by ProSec unit operation:

- Double-click on its icon on the flowsheet or select "Edit..." in the contextual menu
- 2. Press the "Parameters" tab

0

Synopsis

Export...

PARAMETERS CATALYSTS STREAMS FINS

- 3. Press the "Edit..." button
- 4. Press the "Reports" tab

HOME

Import...

Name Validation

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rts" tab	Parameters Reports Scripts Report Streams No	tes Advanced parameters	$\mathbb{C}^{\mathbb{C}}$
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	operation on your computer.	Default calculator	Show a label
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#### • "Simulation" contains the main results:

- $\checkmark$  Report on the input data
- ✓ Results for the "Common Wall Temperature" calculation mode (initialization of ProSec rigorous calculations): inlet & outlet temperatures & vapor fraction, heat duty exchanged
- ProSec results: inlet & outlet temperatures & vapor fraction, heat duty exchanged
- ✓ Pressure drops calculation

✓ ...

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NAME	RATE (kg/s)	VAPOUR INLET	RESULTS A RIGORO FRACTION OUTLET	IBSTRACT	I EMPERI	B )	(J/s)	(kW) -57.1	. !		
NAME ! Hot ! >>SO ! Hot	RATE (kg/s) 1.3 0.1 1.2	VAPOUR INLET 1.0000 1.0000	RESULTS A RIGORO FRACTION OUTLET 1.0000 1.0000	BSTRACT US 1 T A 299.00 285.11	   EMPERJ (K >> >>	B 285.11 285.11 274.17	(J/s) -57051 -16 -45617	(kW) -57.1 -0.0 -45.6			
NAME ! Hot ! >>SO	RATE (kg/s) 1.3 0.1 1.2	VAPOUR INLET	RESULTS A RIGORO FRACTION OUTLET 1.0000 1.0000	BSTRACT DUS I T A 299.00	   EMPERJ (K >> <<	B 285.11 285.11 274.17	(J/s) -57051 -16	(kW) -57.1 -0.0 -45.6 45.6	. ! ) ! ; !		

 "Classes of criteria" shows the number of equations which have a convergence criterion belonging to the class:

10<sup>Class+i</sup> < Criterion value < 10<sup>Class</sup>

This indicates the level of convergence of ProSec.

Name Validation Data Misdistributions Simulation Historic
Data Misdistributions Simulation
Misdistributions Simulation
Simulation
Historic
Convergence
Classes of criteria
Flowrate repartition
^
CLASSES OF THE RESIDUALS
CLASS   NUMBER OF EQUATIONS
BELONGING TO THE CLASS
-6   662 -5   65
-4 1 0
-3   0
-2   0
2 1 0

 "Historic" contains information about the errors (with help if any errors are present) and the topology analysis of the inlet data by the unit operation.

PARAMETERS   CATALYSTS   STREAMS   FINS   REFERENCE LAYERS   INFORMATION PORTS   REPORTS   RESULTS   🔗 VALIDATION
Name
Validation
Data
Misdistributions
Simulation
Historic
Convergence
Classes of criteria
Flowrate repartition
**** DATA TEST OF THE 2 STREAMS ****
**** TEST OF THE STACKING *****
TEST OF THE STRUKING TOTAL
** ABSTRACT TABLE OF PASSAGE NUMBERS BY ZONES
IZ IDIRI ITI
IN IAIDI IITI
STREAM   -1  0  1  2
1   0  0  3  3  6
4   0  0  3  3  6    5   0  0  3  3  6

To consult the reports generated by ProSec unit operation:

 Double-click on its icon on the flowsheet or select "Edit..." in the contextual menu

Numerical parameter

Initialization parame

Result parameters

Document

- 2. Press the "Parameters" tab
- 3. Press the "Edit..." button
- 4. Press the "Results" tab

	ProSec - Unnamed.pmp3 Modified		
generated	<u>File Edit Configuration Flowsheet To</u>	ols <u>S</u> imulation <u>W</u> indows <u>H</u> elp	
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eters" tab	ProSec (\$XTMO)	– O X	
Name: CC	D-PROSEC		
button Desc: Br	azed plate-fin heat-exchanger		
	parameters. Visualize the registered details of the unit operation on your computer. Open the edition window of the unit operation	Thermodynamics Thermo. version 1.1  Output streams calculators Use the same for all streams Default calculator	CC Visual Show a label
CO-PROSEC - CO-ProSec	-	m Model	Move to 🕨
ers eters Conversion Soutput tool Units ERS INFORMATION PORTS			<ul> <li>Bring to front</li> <li>Bring forward</li> <li>Send backward</li> <li>Send to back</li> </ul>
		<u>O</u> K <u>C</u> ancel	

Wall temperature Along a section Along the length

File

Export...

Double-click on a type of curve to visualize

0

Synopsis

PARAMETERS CATALYSTS STREAMS FINS REFERENCE LAY

HOME

Import...

- "Results" tab
  - Graphical results

PARAMETERS | CATALYSTS | STREAMS | FINS | REFERENCE LAYERS | INFORMATION PORTS | REPORTS | RESULTS 🕑 VALIDATION

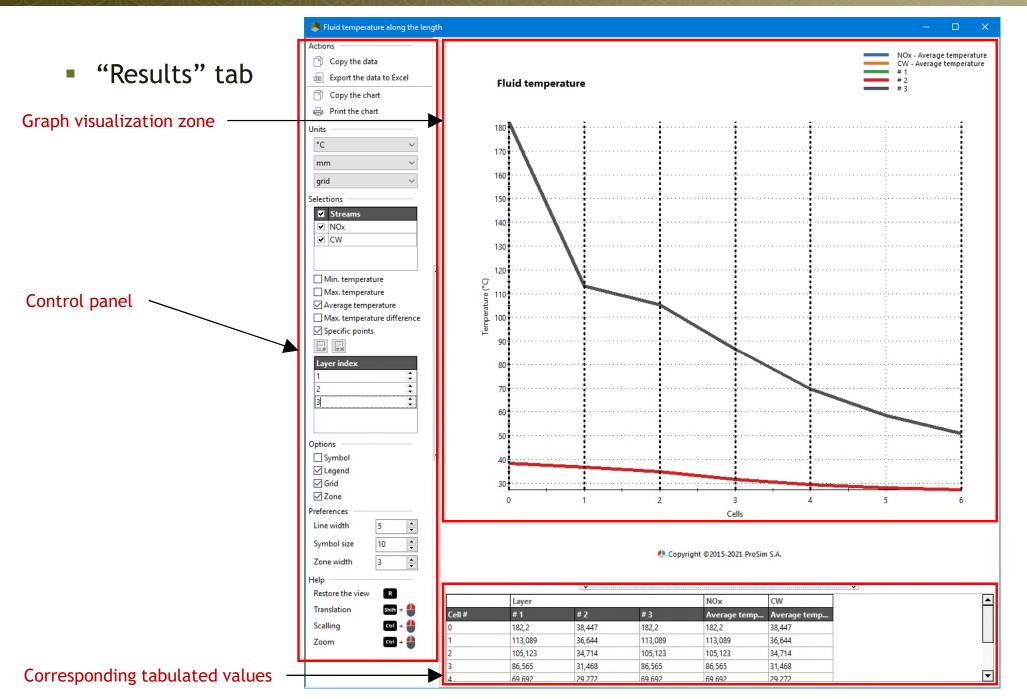
Double-click on a type of curve to visualize

Wall temperature		
Along a section		
Along the length		
Fluid temperature		
Along a section		
Along the length		
Fluid pressure		
Along a section		
Along the length		
Related to the temperature		
Heat transfer coefficients		
Along a section		
Along the length		
Normal efficiency		
Along a section	Double-click on a curve to visualize it	
Along the length		
Enthalpy		
Along a section		
Along the length		
Vaporization ratio		
Along a section		
Along the length		
Holdup		
Along a section		
Along the length		
Flowrate		
Along a section		
Along the length		

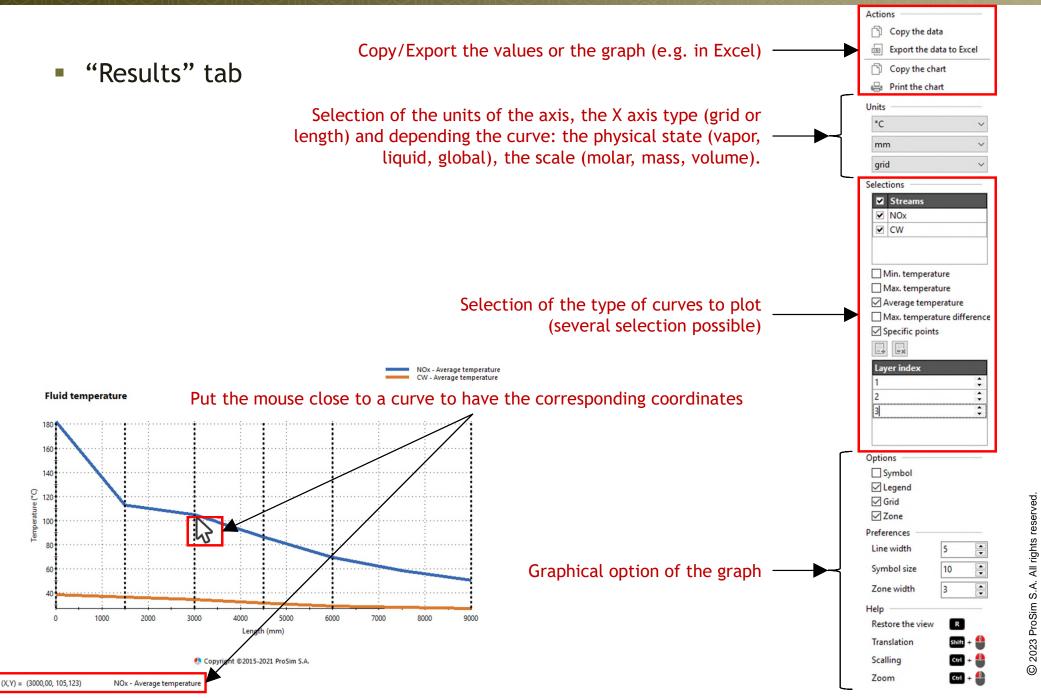
- "Results" tab
  - If at least one stream is vapor-liquid, the properties are displayed, if possible, for the vapor, the liquid and the global physical phase.
  - In green, available only for ProSec Reaction
  - In Prosec Reaction, the properties are displayed, if possible, in molar, mass and volume scale.

	Wall temperature	Friction factors	
	Along a section	Along a section	
	Along the length	Along the length	
	Fluid temperature	By-pass efficiency	
	Along a section	Along a section	
	Along the length	Along the length	
es	Fluid pressure	Reactions	
	Along a section	Vapor rates along the length	
	Along the length	Vapor extents along the leng	
	Related to the temperature	Exchanged heats	
	Heat transfer coefficients	Along a section	
	Along a section	•	
	Along the length	Along the length	
	Normal efficiency		
	Along a section		
	Along the length		
f	Enthalpy		
· · · ·	Along a section		
	Along the length		
	Vaporization ratio		
	Along a section		
	Along the length		
	Holdup		
	Along a section		
	Along the length		
	Flowrate		
	Along a section		
	Along the length	_	
	Fractions		
	Along the length		
	Velocity		
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	Dynamic viscosity		Ē
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	Along the length		2023 ProSim S.A. All rights reserved
	Thermal conductivity		Sin
	Along a section		Pro
	Along the length		)23
	Reynolds number		0 20
	Along a section	(	0

Along the length



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- "Results" tab
  - Display of 3D curves

simulation file) to have access to the 3D curves. All the data will be saved in the "csv" file you will HOME specify. Numerical parameters 0 < Input Plaitialization parameters Conversion 🙈 Output Synopsis Import... Export... Result parameters tool File Document Units Curves parameters Curves Curves data embedding C: \Users \rodolphe sardeing \Desktop \Nouveau dossier \3Dcurves.csv 3D curves data generation (\*) Temperatures Velocity Pressure Density Heat transfer coefficient Dynamic viscosity Normal efficiency Thermal conductivity Enthalpy Reynolds Vaporization ratio Friction factor Holdup FBy-pass efficiency For simulations with a high number of Exchanged heat ✓ Flowrate streams and/or meshes, the curves (\*) only when curves data are not embedded could be not displayed. In that case, Restore Ok Cancel just decrease the number od 3D curves.

Deactivate the "Curves data embedding" (in the

# Step 5: Reports generated C- ProSimPlus general reports

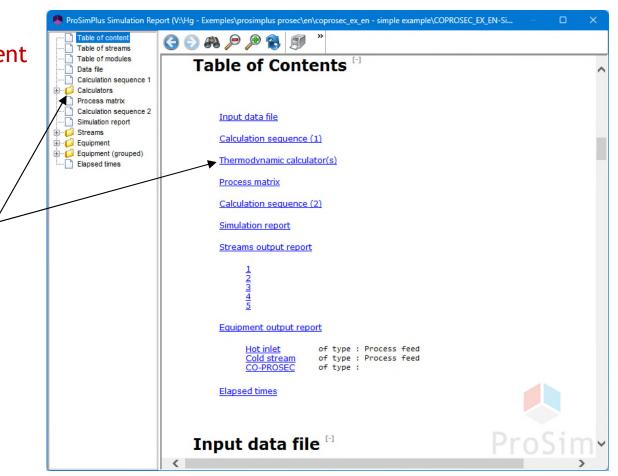
The HTML report is by default automatically displayed after each run.

It provides information about:

- Pure component properties and thermodynamic models
- List of equipment calculation
- Process streams characteristics
- Results for each process equipment
- Convergence and constraints

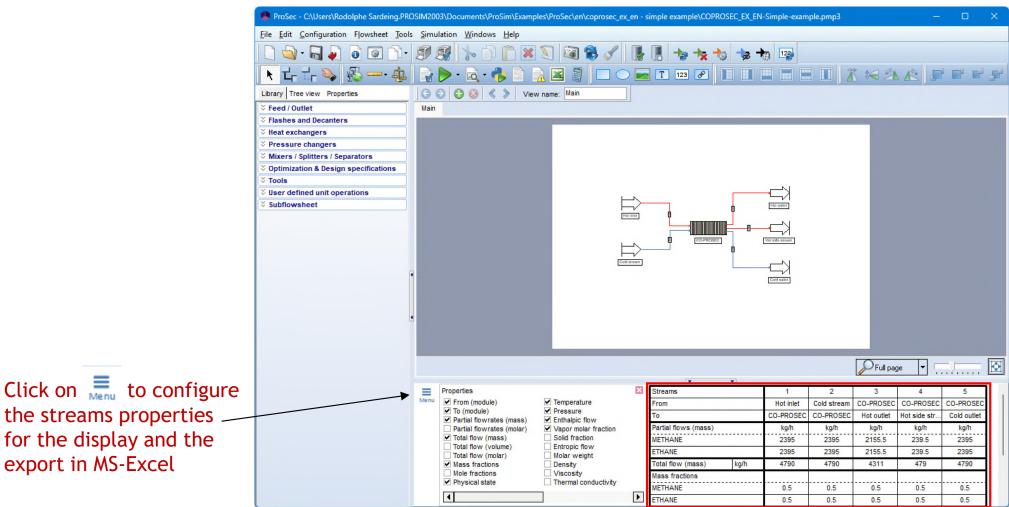
Hyperlinks give you direct access to detailed information on initial configuration, unit operations, calculation sequence and results.

All the reports are created in the folder where you saved your project.



# Step 6: Analyze simulation results from the flowsheet

#### A table with selected results is automatically generated and located below the flowsheet.



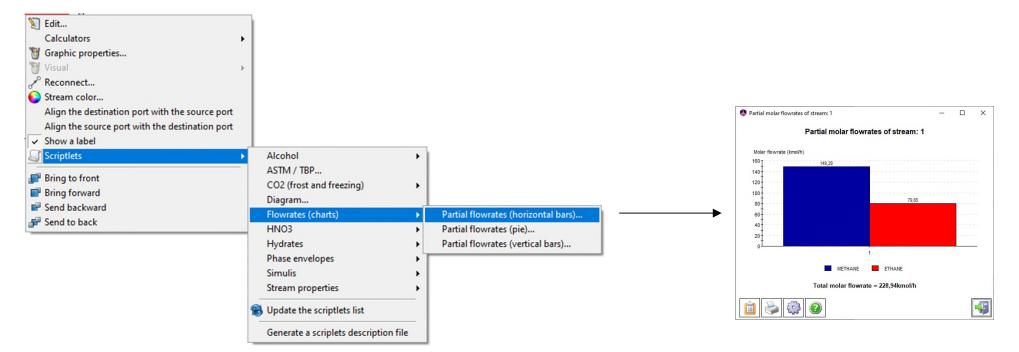
You can copy the grid to paste it in other documents or directly export it to an Excel file.

77

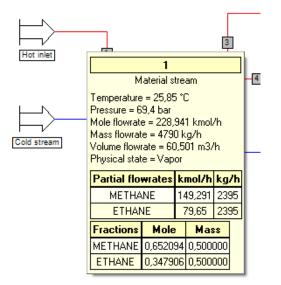
# Step 6: Analyze simulation results from the flowsheet

In the drawing area, positioning the mouse on a stream displays its characteristics

Right click on a stream to access the contextual menu. With Scritplets, you can analyze results through different types of charts.



#### These charts can be copied and pasted in other documents

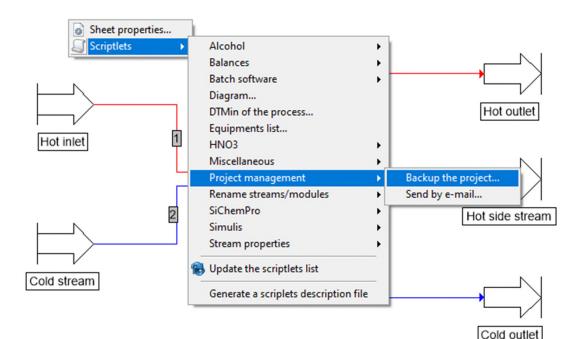


# Step 7: Sharing the simulation

When you need to send the simulation to someone else, simply right click anywhere on the flowsheet, and select the Scriptlet "Send by e-mail...".

This action will automatically create a zip file that will include among other:

- ✓ The ".pmp3" file (ProSimPlus file)
- $\checkmark\,$  The History file









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