

Process Simulation: The Need for an Advanced Thermophysical Calculation Server



26th ESAT – 06-10 October, 2012
Kongresshotel Potsdam (Germany)
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① Simulis® Thermodynamics: a Thermophysical calculation server

Computes thermophysical properties and phase equilibria on pure components or mixtures:

PROPERTIES CALCULATED

Transport properties

- Isobaric specific heat (Cp)
- Dynamic viscosity
- Thermal conductivity
- Density
- Molar Volume
- Molar density
- Surface tension
- Molecular weight

Liquid-Vapor equilibria

- Bubble and dew temperatures and pressures
- Flash at given temperature (T) and pressure (P)
- Flash at given vaporization ratio and P (or T)
- Flash at given enthalpy (H) and P (or T, or V, or U)
- Flash at given entropy (S) and P (or T, or V, or H, or U)
- Flash at given internal energy (U) and P (or T, or V)
- Flash at given volume (V) and P (or T)
- Phase Envelope

Compressibility properties

- Compressibility factor
- Gamma (Cp/Cv ratio)
- Sound speed

Liquid-Liquid equilibria

- Flash at given temperature and pressure

Liquid-Liquid-Vapor equilibria

- Bubble temperature
- Flash at given enthalpy and pressure
- Flash at given temperature and pressure
- Flash at given vaporization ratio and pressure

Thermodynamic properties

- Enthalpy (H)
- Entropy (S)
- Internal energy (U)
- Isochoric specific heat (Cv)
- Enthalpy of vaporization

Non-ideal properties

- Activity coefficients
- Fugacity coefficients and Fugacity

Derivatives of the properties with respect to temperature, pressure and number of moles are also provided

THERMODYNAMIC MODELS AVAILABLE

Equations of State

- Soave-Redlich-Kwong (SRK)
- Peng-Robinson (PR)
- Lee-Kesler-Plöcker (LKP)
- Predictive Peng-Robinson 78 (PPR78)
- NRTL-PR
- PPC-SAFT
- etc...

Activity coefficients models

- NRTL
- UNIQUAC
- UNIFAC (Larsen, Dortmund,...)
- Wilson
- etc...

Combined approach models

- MHV2
- MHV1
- PSRK
- etc...

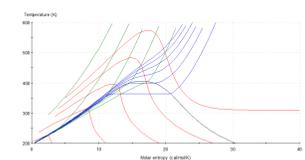
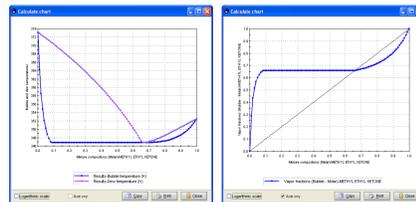
Specific systems

- Pure Water
- Amines
- Sour-Water
- Formaldehyde
- etc...

Electrolytes

- Edwards
- UNIQUAC electrolyte
- ULPDHS
- etc...

The various available methods can be combined in order to configure a thermodynamic model adapted to a specific system



A full set of services available:

- Data regression of experimental properties
- Graphical display of properties on temperature, pressure or composition ranges
- Generation of property tables
- Export of PSF files (HTFS), PVT files (OLGA)
- Estimation of pure component properties
- Plot of phase envelope diagrams
- Residue curves calculation & ternary diagrams
- Calculation of petroleum fractions properties
- Unit conversions
- Predictive models manager (UNIFACs, PPR78, NRTL-PR...)
- etc...

All these services become automatically available in your usual software since it embeds Simulis® Thermodynamics

Uses the widely validated thermodynamic library of ProSim:

- Maturity of the architecture
- Reliability of the results
- Robustness of algorithms

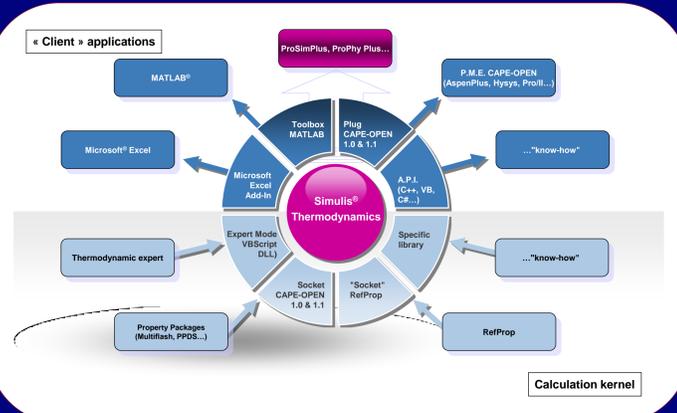
Supplied with a database of over 2 000 components including AICHE's DIPPR® database and access to your "private" databases of pure components properties.



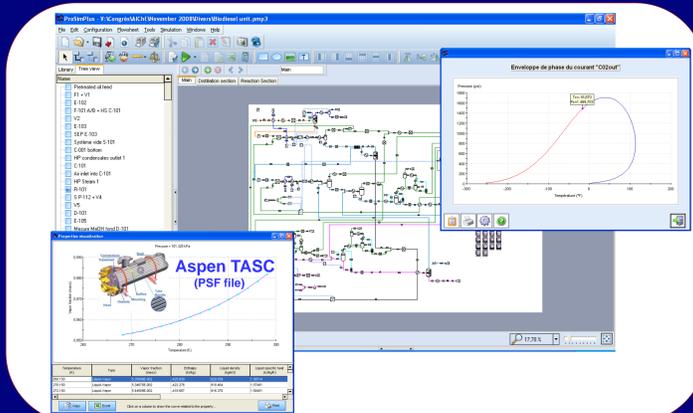
Other software components included:

- Simulis® Conversions: physical units conversion management tool
- Simulis® Properties: pure substances properties server

② Easy to embed in your environment



Any application that integrates Simulis® Thermodynamics automatically inherits from its CAPE-OPEN standard compliance



③ "Expert mode" to add your own thermodynamic models (new or existing ones)

Dynamic Link Library (DLL)



VBScript

Capability to use legacy codes

End-users can introduce their own know-how within Simulis® Thermodynamics

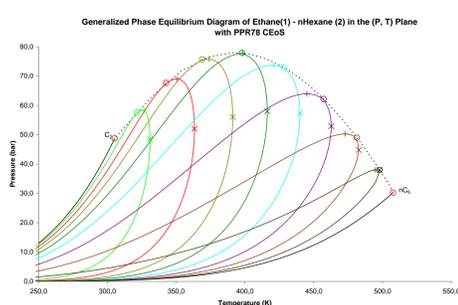
Ability to merge native ProSim codes and legacy codes.

Ability to use native pure compound properties in legacy codes.

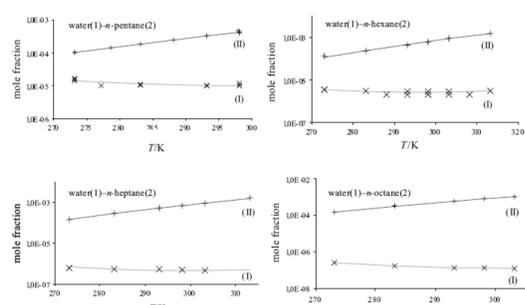
Tests and debugging facilities supplied to developers

④ Thermodynamic library enriched every year

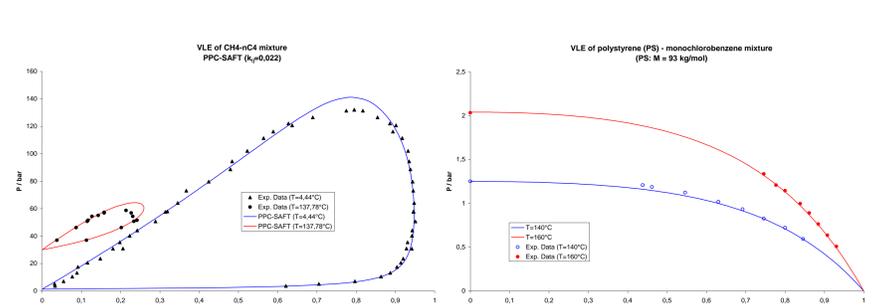
PPR78 [1 - 4]



NRTL-PR [5 - 7]



PPC-SAFT [8 - 11]



[1] JAUBERT J.N., MUTELET F., Fluid Phase Equilibria, vol. 224, pp. 285-304 (2004)
[2] JAUBERT J.N., VITU S., MUTELET F., Fluid Phase Equilibria, vol. 237, pp. 193-211 (2005)
[3] JAUBERT J.N., VITU S., MUTELET F., Fluid Phase Equilibria, vol. 243, pp. 9-28 (2006)
[4] PRIVAT R., JAUBERT J.N., MUTELET F., J. Chem. Thermodynamics, vol. 40, pp. 1331-1341 (2008)

[5] ESCANDELL J., PhD Thesis (2008)
[6] NEAU E., ESCANDELL J., NICOLAS C., Ind. Eng. Chem. Res., 49, pp. 7580-7588 (2010)
[7] NEAU E., ESCANDELL J., NICOLAS C., Ind. Eng. Chem. Res., 49, pp. 7589-7596 (2010)

[8] D. NGUYEN HUYNH, A. FALAIX, JP PASSARELLO, P. TOBALY, JC de HEMPTINNE, Fluid Phase Equilibria, 264 (1), 184-200 (2008)
[9] D. NGUYEN HUYNH, JP PASSARELLO, P. TOBALY, JC de HEMPTINNE, Fluid Phase Equilibria, 264 (1-2), 62-75 (2008)
[10] D. NGUYEN HUYNH, JP PASSARELLO, P. TOBALY, JC de HEMPTINNE, Industrial & Engineering Chemistry Research 47 (22), 8847-8858 (2008)
[11] D. NGUYEN HUYNH, JP PASSARELLO, P. TOBALY, JC de HEMPTINNE, Industrial & Engineering Chemistry Research 47 (22), 8859-8868 (2008)